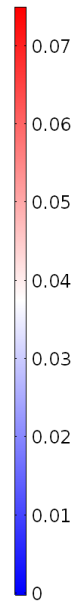
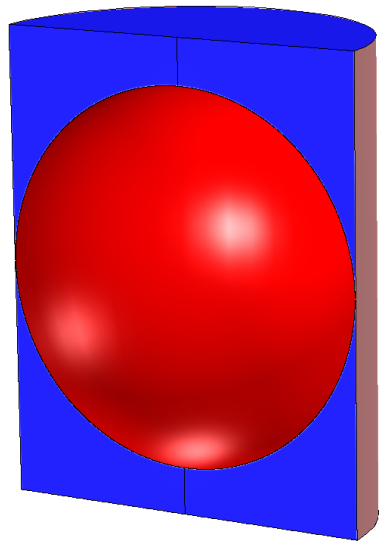


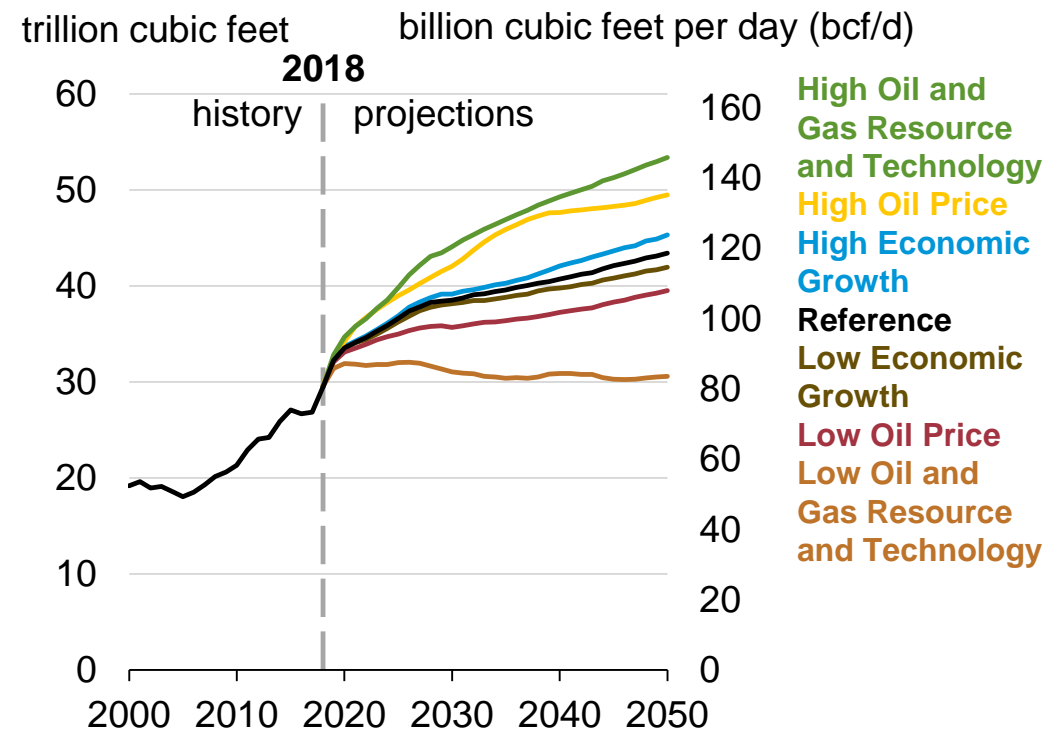
Electrostatic Interactions Between Charged Bubble Interface and Solid Wall



Jonathan C. Hui, Peter Huang
Binghamton University, State University of New York
COMSOL Conference Boston
October 3, 2019

Projected U.S. Natural Gas Consumption & Production

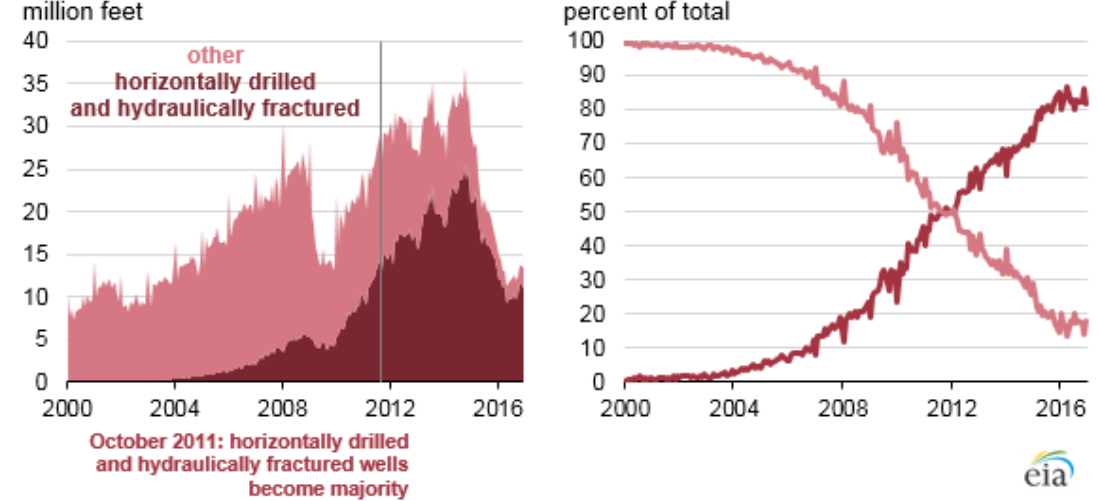
Dry natural gas production



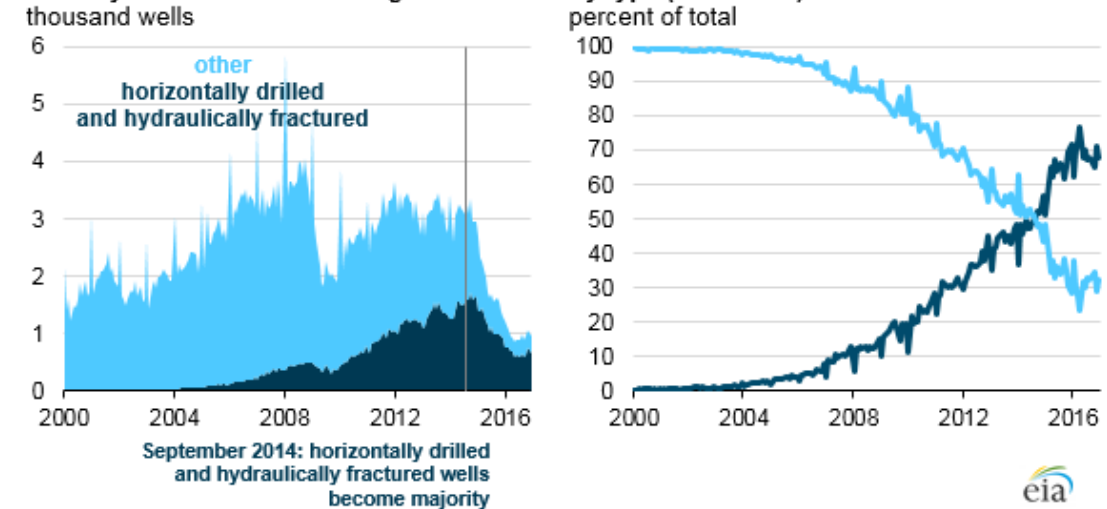
Source: U.S. Energy Information Administration Annual Energy Outlook 2019

- Increase in production and consumption through next 30 yrs
- International Energy Agency: 2018 record high production of 139 tcf (4% increase from 2017)
- Hydraulic fracturing has become predominant method of extracting gas since 2011 and accounted for most of all new wells drilled since late 2014

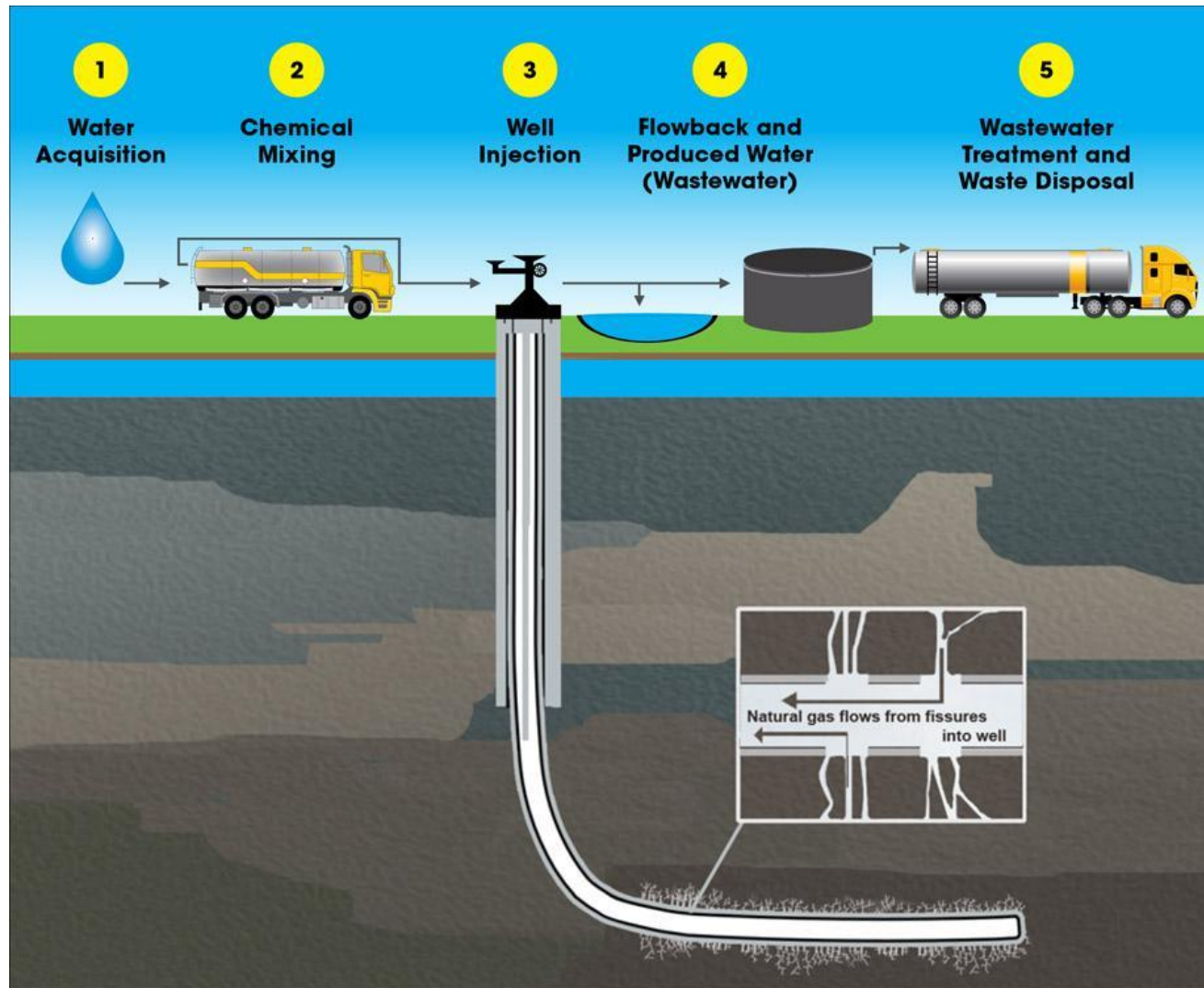
Monthly crude oil and natural gas well drilling footage by type (2000-2016)



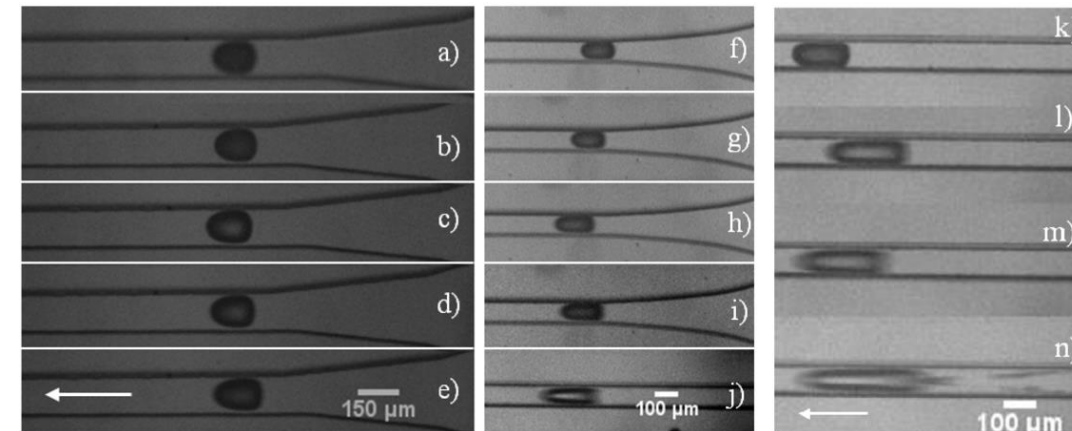
Monthly crude oil and natural gas well count by type (2000-2016)



Hydraulic Fracturing Overview

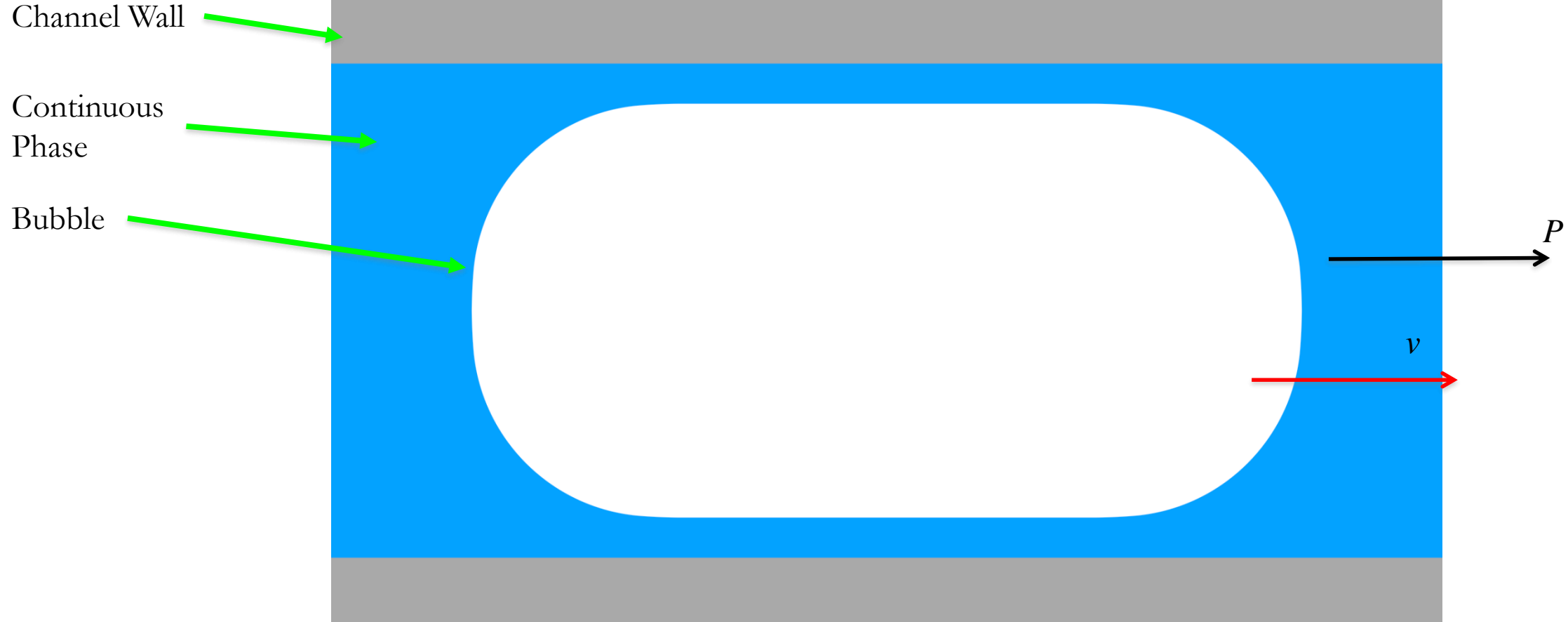


Source: U.S. Environmental Protection Agency

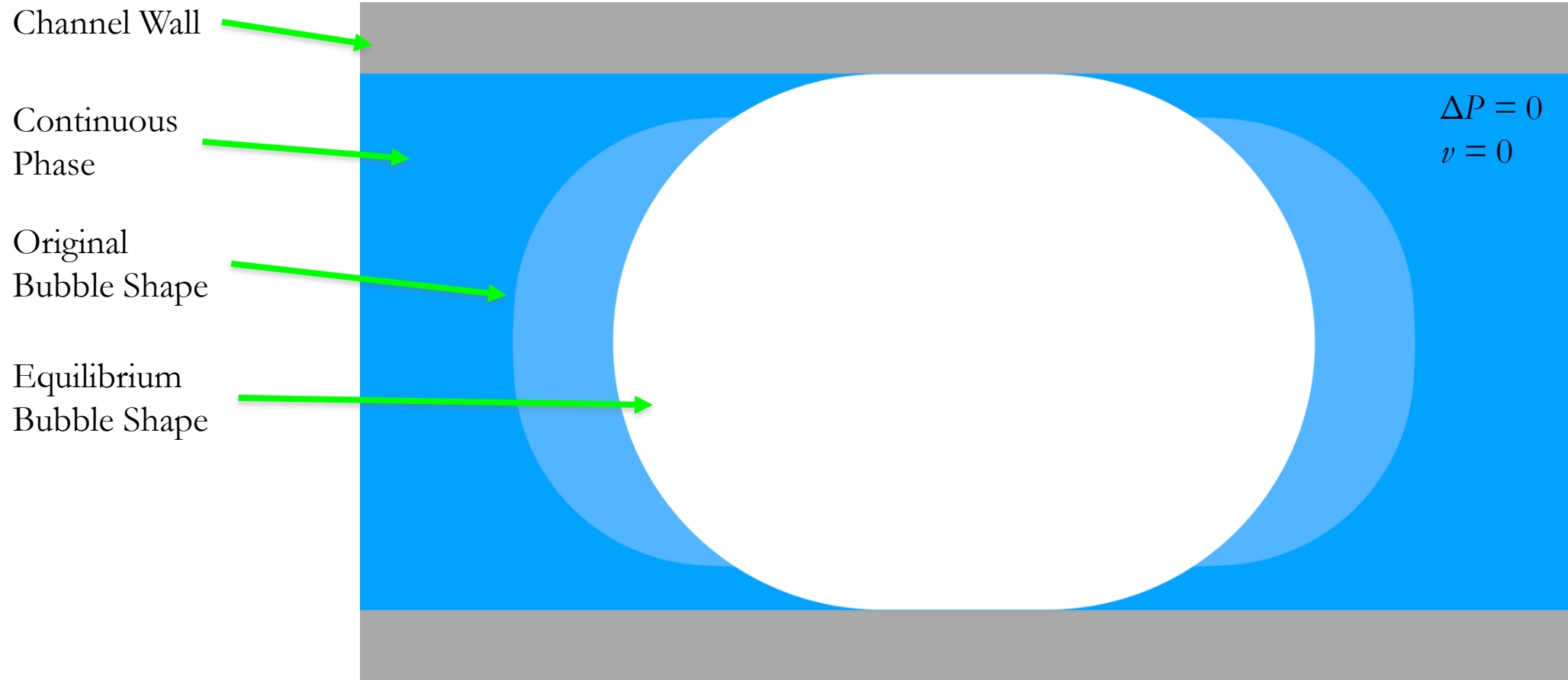


Source: M. K. Mulligan and J. P. Rothstein. *Deformation and Breakup of Micro- and Nanoparticle Stabilized Droplets in Microfluidics Extensional Flows*. *Langmuir*, 27(16):9760–9768, July 2011

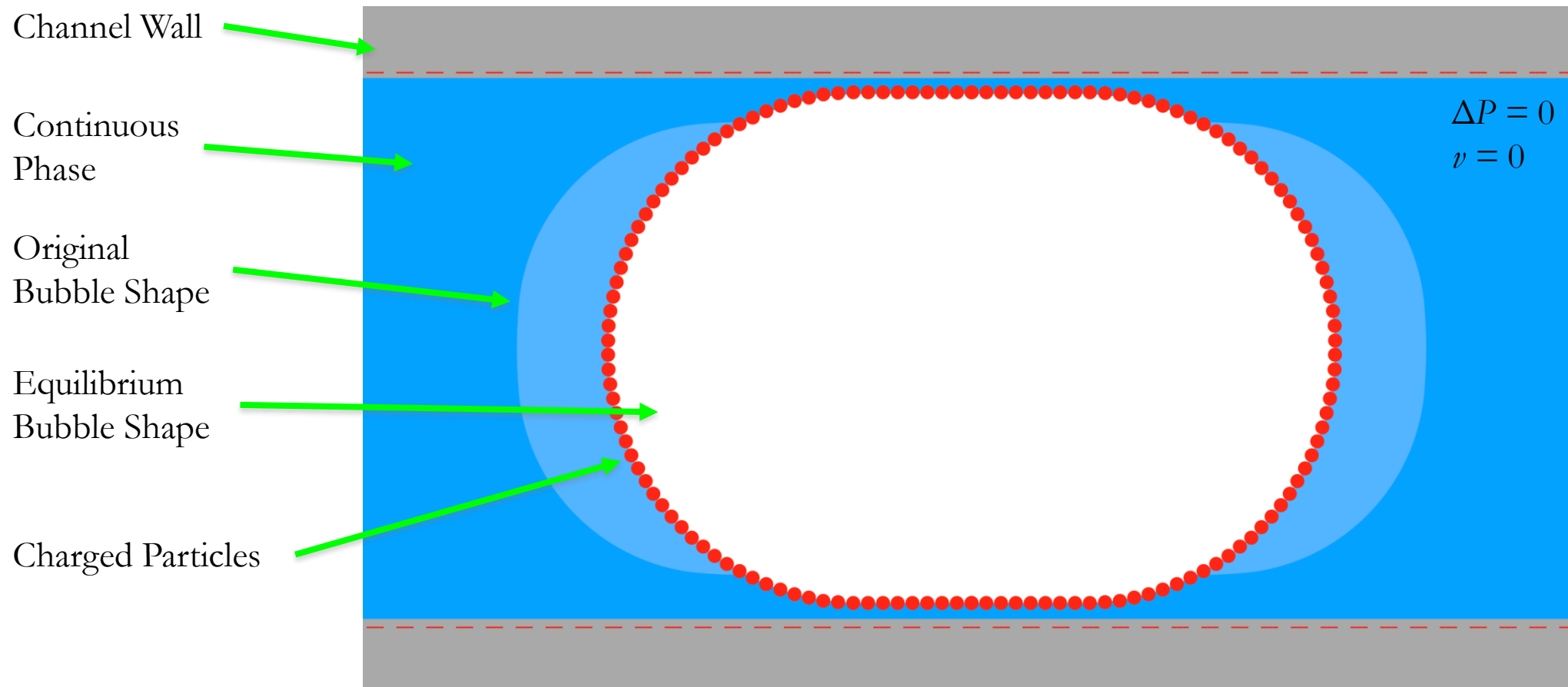
Problem



Problem



Problem



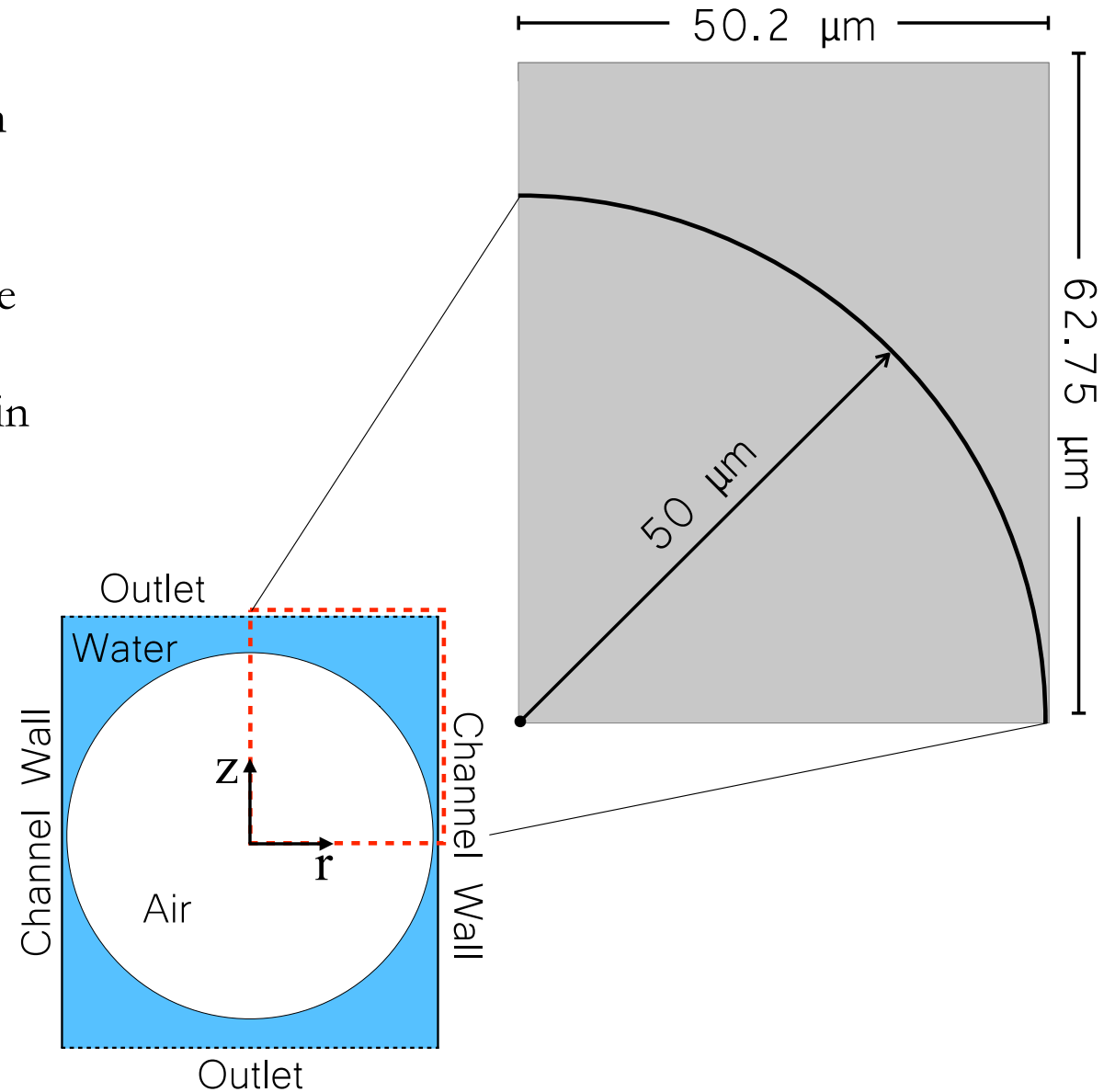
Deformation and Contact Considerations:

- Surface Tension
- Disjoining Pressure
- Electrostatic Forces

Model – Geometry

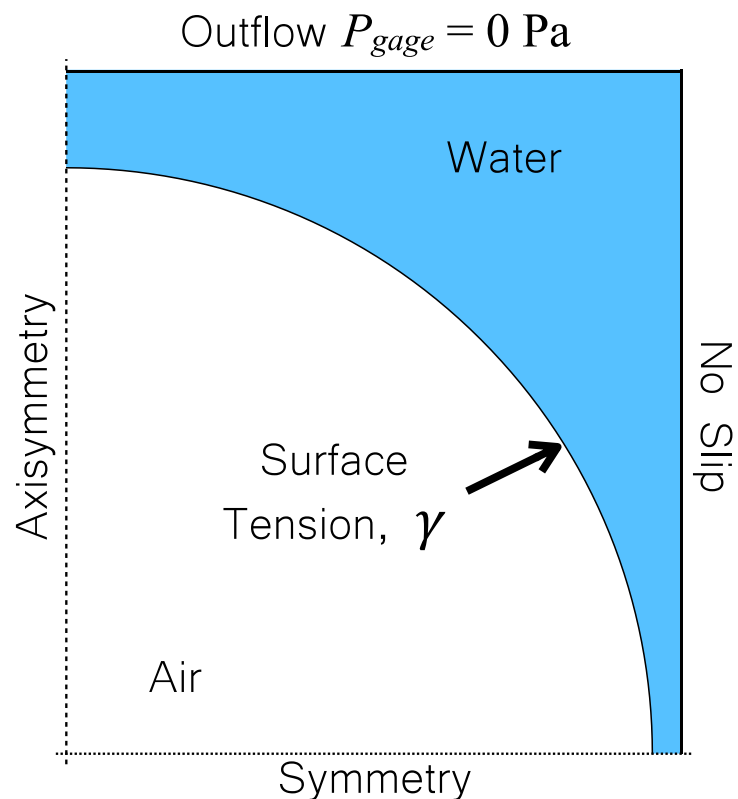
Objectives:

- Find conditions of maximal electrostatic repulsion between bubble interface and channel wall
- Simulate bubble morphology due to electric charge effects from channel wall on spherical bubble interface using the customized weak contribution in COMSOL
- Spherical bubble in microchannel
- 2D axisymmetry & planar symmetry
- Initial bubble radius = $50\mu\text{m}$
- Channel radius = $50.2\mu\text{m}$
- Half channel height = $62.75\mu\text{m}$



Model – Boundary Conditions

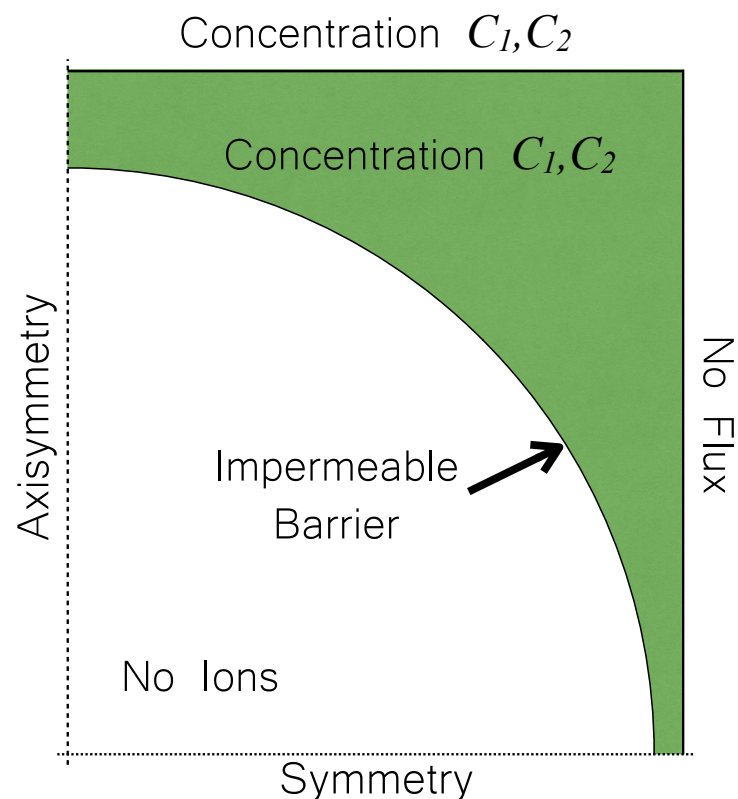
Fluid



$$\rho \nabla \cdot \vec{u} = 0$$

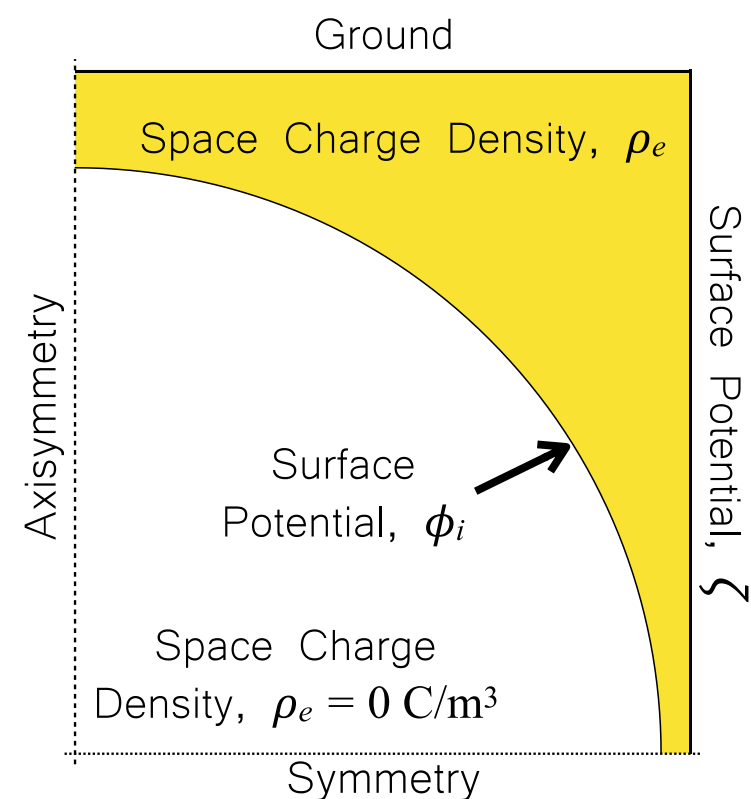
$$\rho \frac{\partial \vec{u}}{\partial t} + \rho (\vec{u} \cdot \nabla) \vec{u} = \nabla \cdot [-p \vec{I} + \mu (\nabla \vec{u} + (\nabla \vec{u})^T)] + \vec{F}$$

Transport of Dilute Species



$$\frac{\partial c}{\partial t} + \nabla \cdot (-D \nabla c_j) + \vec{u} \cdot \nabla c_j = R_j$$

Electrostatic



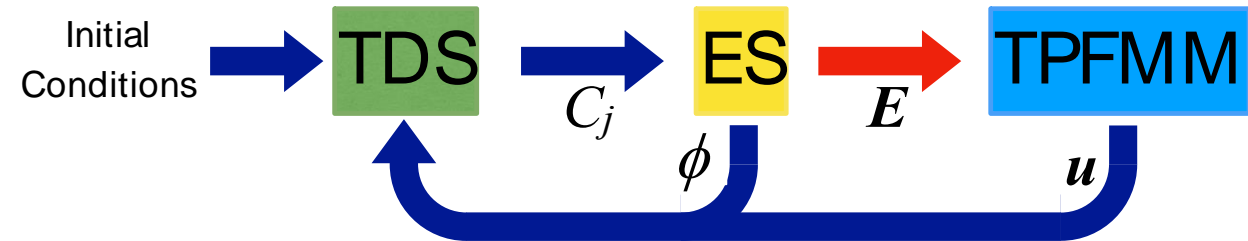
$$\nabla \cdot \vec{D} = \rho_e$$

Model – Module Implementation & Weak Formulation

- Two Phase Flow Moving Mesh Method (TPFMM) – Multiphase, interfacial tracking
- Transport of Dilute Species module (TDS) – Ion concentration
- Electrostatics module (ES) – Electric field

$$\rho \left[\frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \vec{u} \right] = \nabla \cdot \bar{\bar{\sigma}}$$

Navier-Stokes Eqn



$$\hat{n} \cdot (\bar{\bar{\sigma}}_A - \bar{\bar{\sigma}}_B) = \Gamma \gamma \hat{n} - \nabla_s \gamma - \rho_s \nabla \phi$$

Boundary Condition at Fluid-Fluid Interface

Total Stress

With unit normal from gas B to liquid A

Surface Tension

Electrostatics

Weak Form

$$\int_{\Omega} \rho \left[\frac{\partial \vec{u}}{\partial t} + (\vec{u} \cdot \nabla) \vec{u} \right] \cdot \vec{v} d\Omega = - \int_{\Omega} \nabla \vec{v} : \bar{\bar{\sigma}} d\Omega + \int_S \gamma (\nabla_s \cdot \vec{v}) dS - \int_S \vec{v} \cdot \rho_s \nabla \phi dS.$$

Time Deriv

Advection

Diffusion

Surface Tension BC

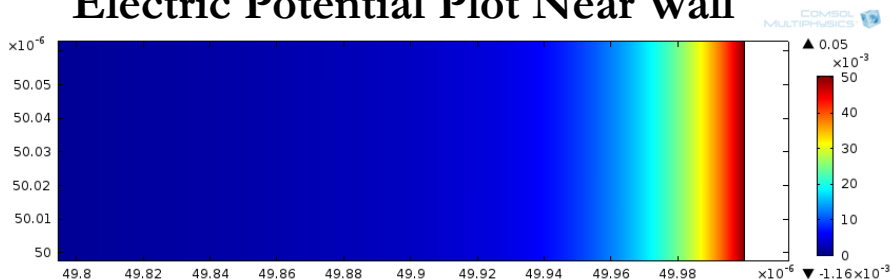
Electrostatic BC

Implemented as
Weak Contribution for **E**

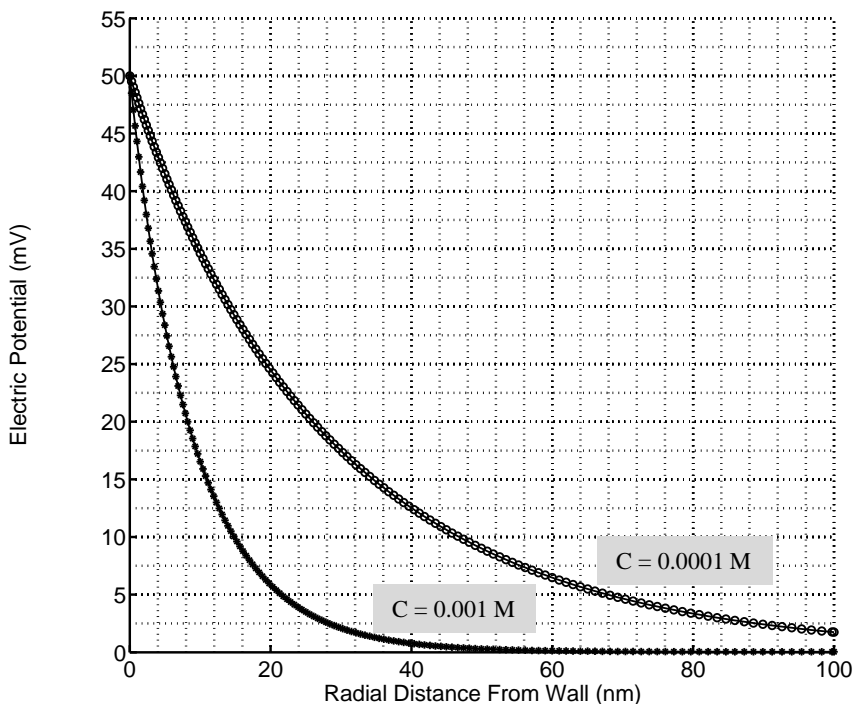
Results – Electric Double Layer

Verify COMSOL Capability for Steady State EDL Profile

Electric Potential Plot Near Wall



Electric Potential Profile Away from Wall



Numerical Debye Length

$$\psi(x) = \zeta e^{-x/\lambda} \quad (\text{Boltzmann distribution})$$

$$\ln \psi = -\frac{1}{\lambda}x + \ln \zeta$$

Theoretical Debye Length

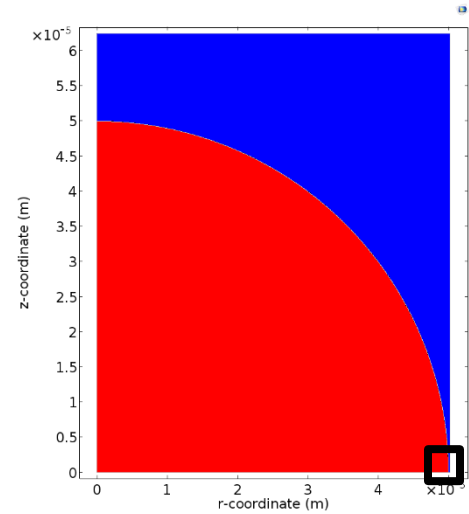
$$\lambda = \left(\frac{F^2}{\epsilon \epsilon_0 RT} \sum_i z_i^2 C_{i,b} \right)^{-1/2} \quad (\text{Debye-Huckel approximation})$$

$$\lambda = \left(\frac{2C_b F^2}{\epsilon \epsilon_0 RT} \right)^{-1/2} \quad (\text{Univalent-Univalent, Symmetric Electrolyte})$$

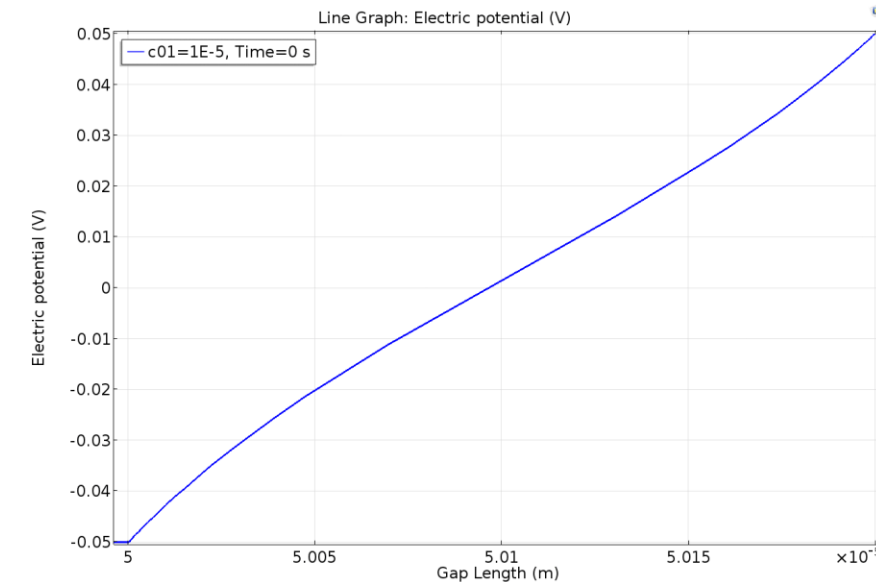
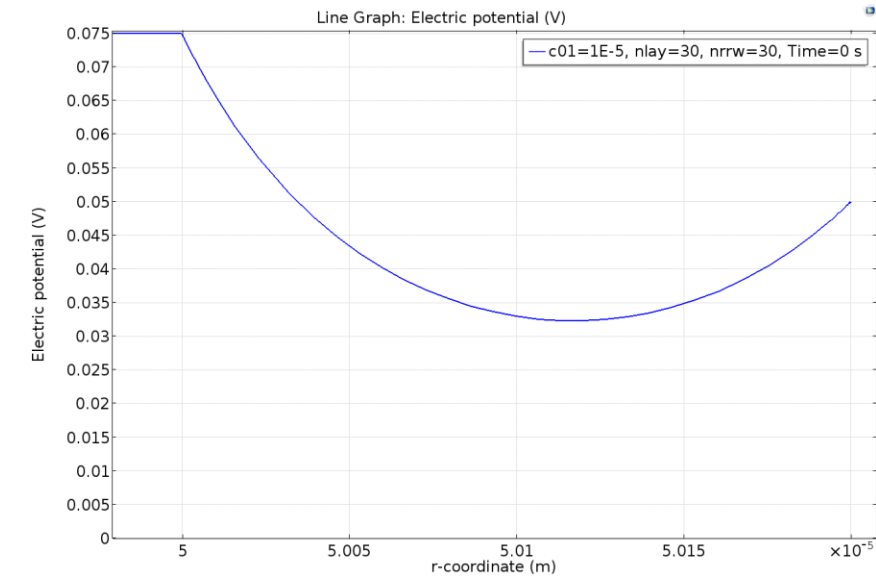
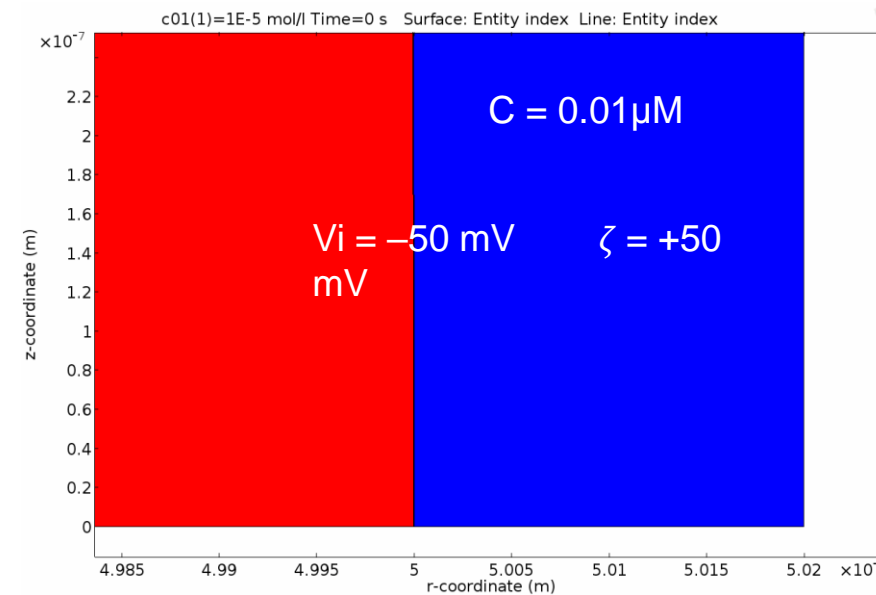
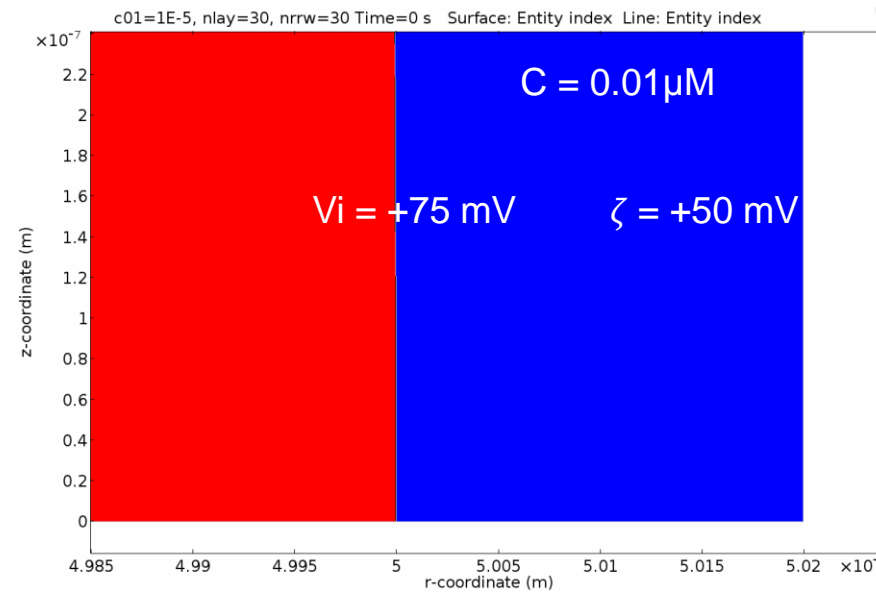
C (M)	λ_{nm} (nm)	λ_{th} (nm)	$\frac{\lambda_{th} - \lambda_{nm}}{\lambda_{th}} \cdot 100$
0.001	9.60	9.63	0.3
0.0001	29.9	30.4	1.6

Strong Theoretical & Numerical Agreement

Results – Repulsion/Attraction

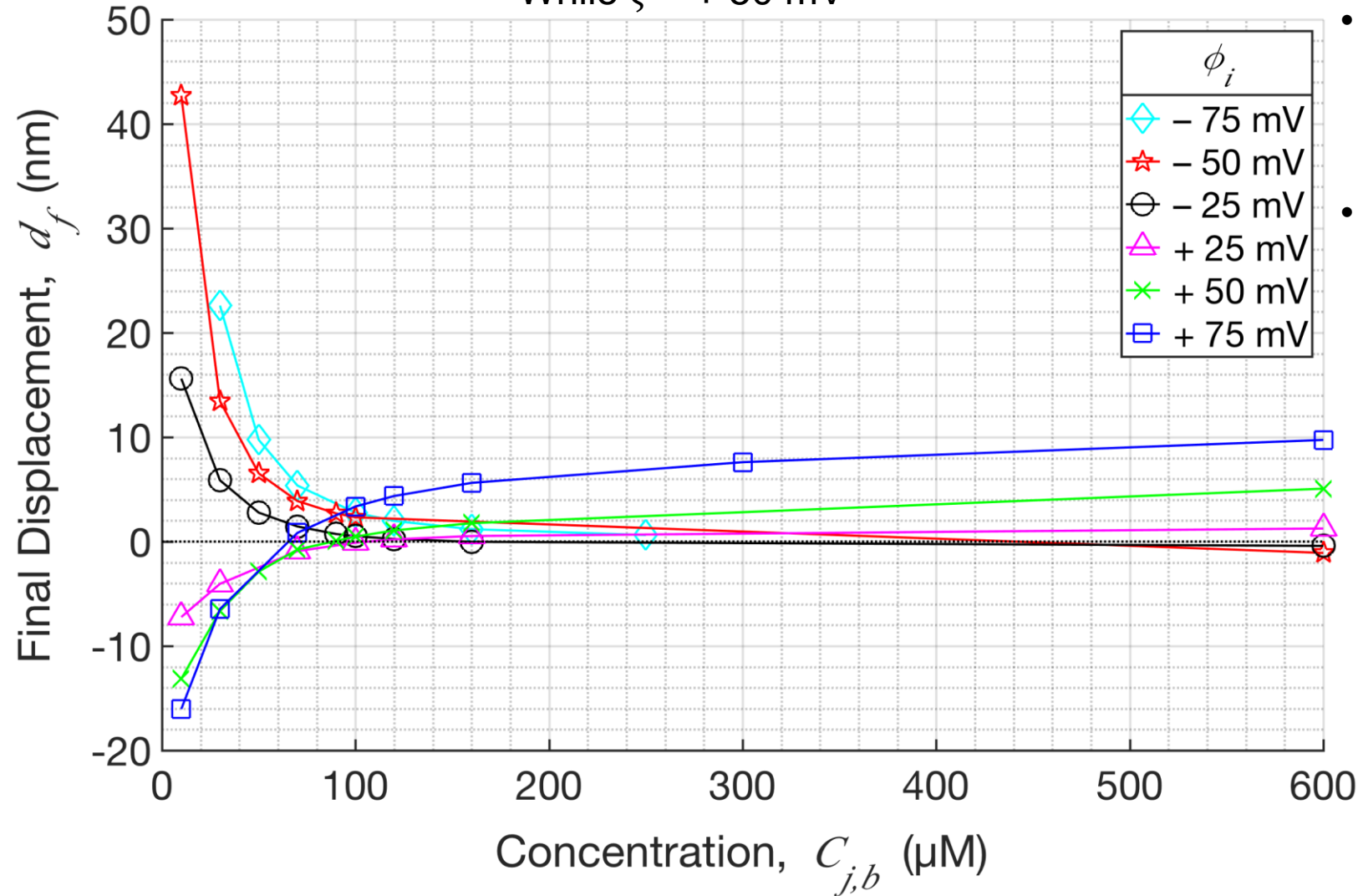


- Repulsive behavior with like electric potential
- Attractive behavior with unlike electric potential
- Double layer overlapped and updated through time

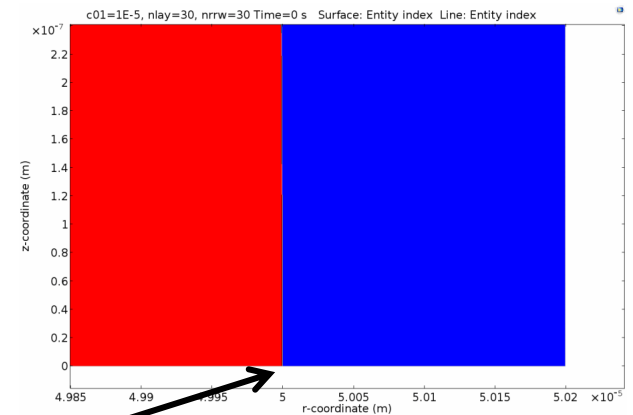


Results –Attraction/Repulsion

Final Displacement vs. Concentration at Various Interfacial Potential
While $\zeta = + 50$ mV

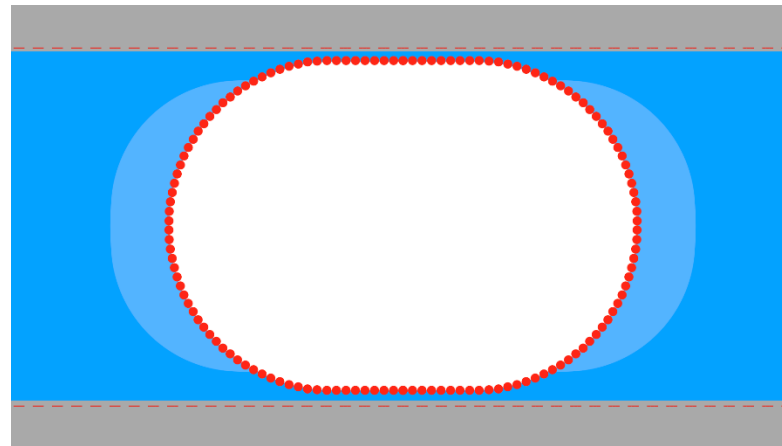


- Unlike Potential
 - Attractive behavior for low concentration
 - Neutral behavior for high concentration
- Like Potential
 - **Repulsive behavior for low concentration**
 - Attractive behavior for high concentration



Conclusion

- Developed a customized model to couple electrostatic influence on bubble interfacial morphology
- Quantify repulsive and attractive interactions between charged bubble interface and charged channel wall
- Key parameters: Electric potential and ion concentration for a given geometry
- Below certain ionic concentration threshold, larger electric potentials of like polarity maintain thicker lubrication layers
- Ability to create repulsive environments indicates strong possibilities for precluding bubble contact



Acknowledgements:

American Chemical Society

Binghamton University, State University of New York