

Thermal Design of Lithium Sulfur Batteries

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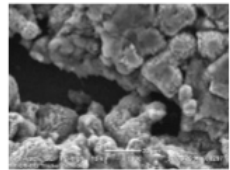
OXIS Energy

COMSOL Conference, Munich 2016

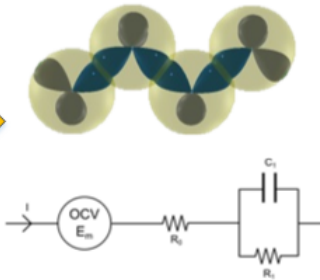
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Model led R&D approach at OXIS

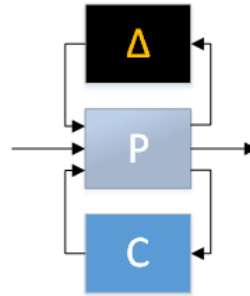
Goal : To develop a battery module demonstrator



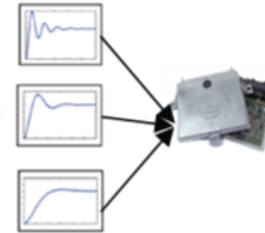
Materials research & cell design



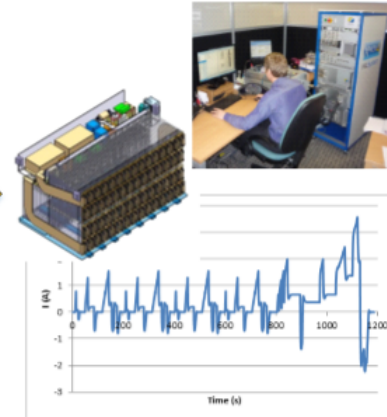
Lithium Sulfur chemistry modelling



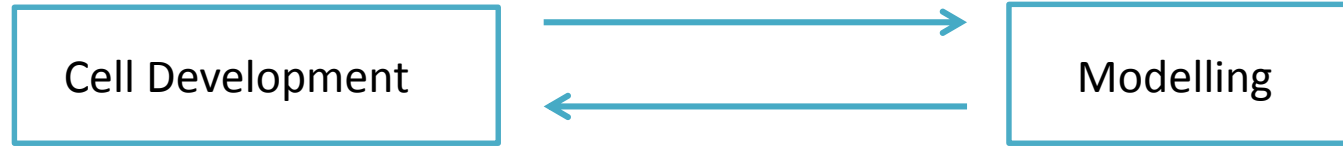
Control algorithms



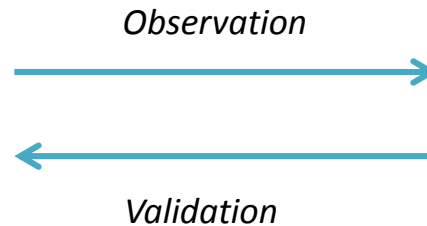
Control Hardware



Battery Testing



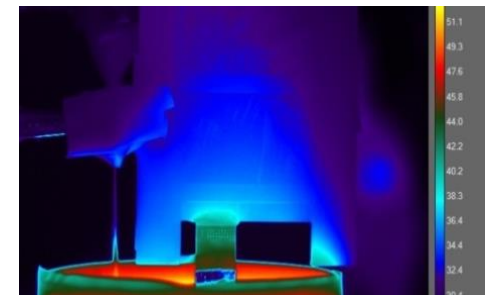
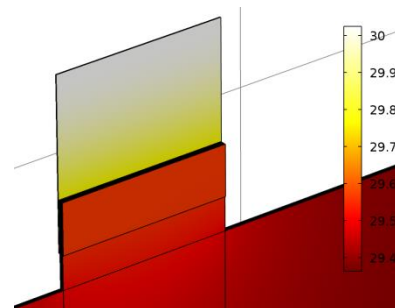
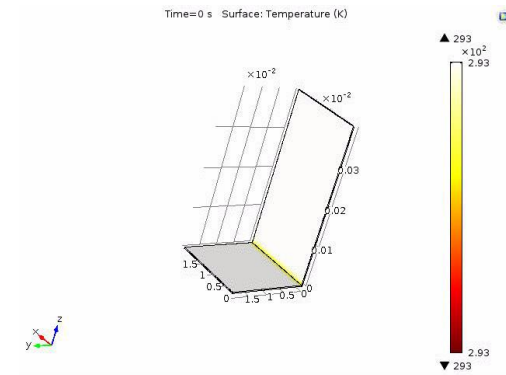
REVB takes the best of current materials research at OXIS and puts that into a cell



Modelling allows us to gain a more fundamental understanding of mechanisms : predict and optimise with minimal experiments

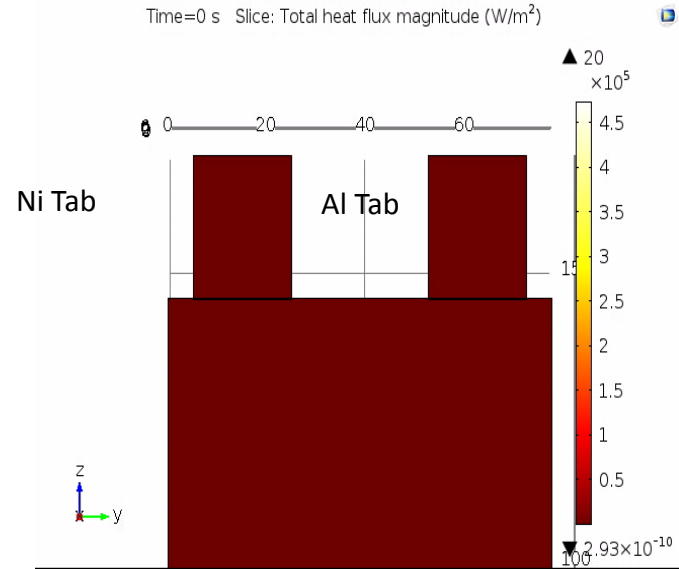
An example of this is thermal management of automotive cells : How do we investigate and mitigate increased heat generation ?

- Testing cells at high temperatures is expensive and potentially risky
- For automotive thermal management is essential
- Modelling is a perfect method for analysis of many different scenarios and cherry picking only certain cases to validate and test : **COMSOL is ideal in its versatility!**
- We look at it from all scales : from the cell to the battery pack



- **Cell Design : Weld resistance**
- Battery Pack : Polysulfide shuttle and thermal runaway
- Pack Integration : Laminar Flow

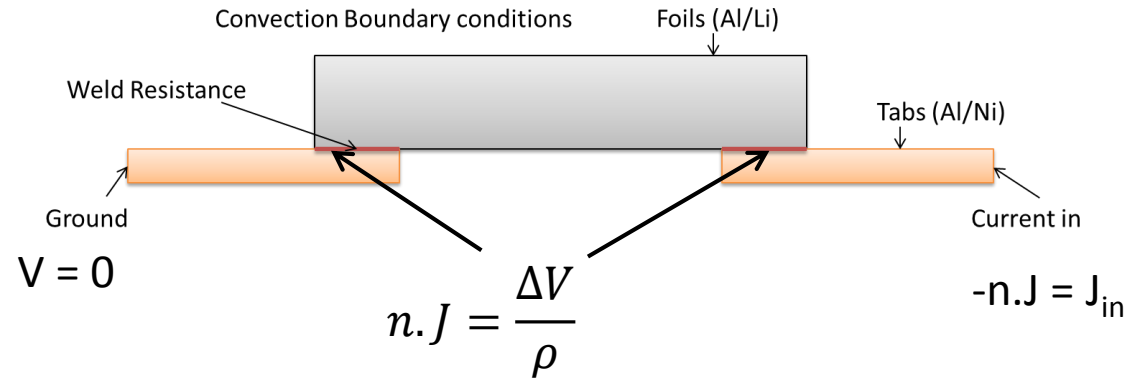
- Li-s cells consist of alternating layers of cathodes and anodes
- Current collectors (positive electrode) are welded to aluminium tabs
- Anodes (No current collectors for negative electrode) are welded to nickel tabs
- As we increase the cell capacity we increase the number of layers
- Qs : Will current methods at use in OXIS lead to increased Joule heating at the tabs and at the weld points ?
- Qs : Will this affect heat flow out of the cell?

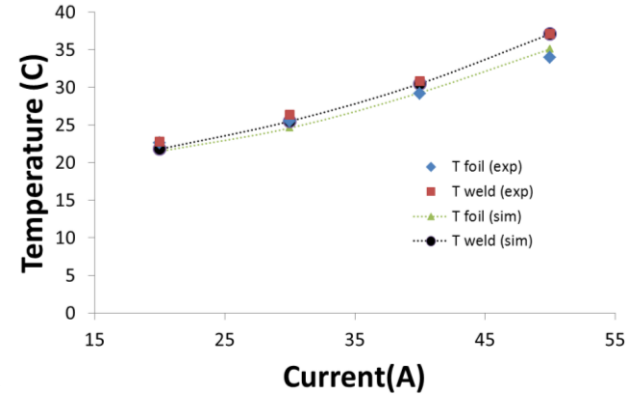
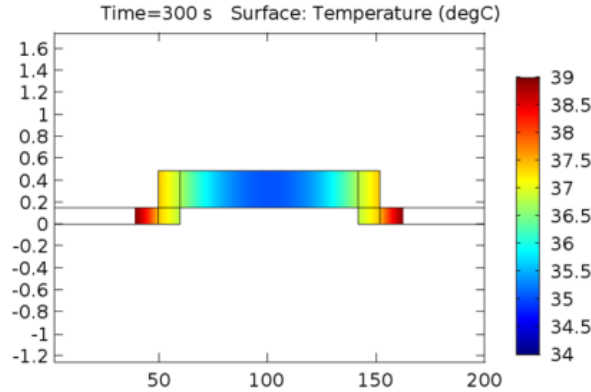
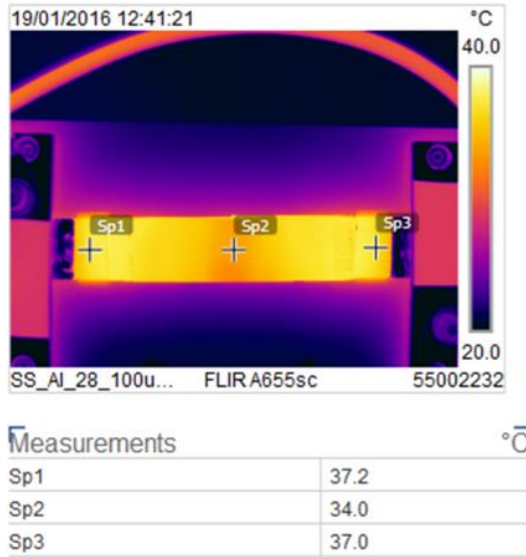


- 2D model used : mimics coupon design used in experiment
- In-built Joule Heating module
- Current Conservation + Heat Transfer in Solids : Multiphysics Coupling
- A surface impedance is applied between the foils and the tabs
- Two systems are analysed : Al tabs and Al foils, and Ni tabs and lithium foils

$$\nabla \cdot J = 0$$

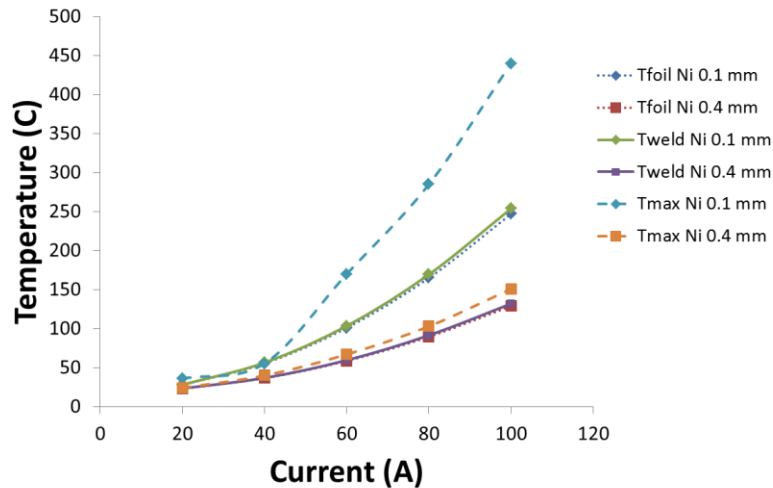
$$\rho C_p \frac{dT}{dt} + \nabla \cdot (-k \cdot \nabla T) = Q_{elec}$$





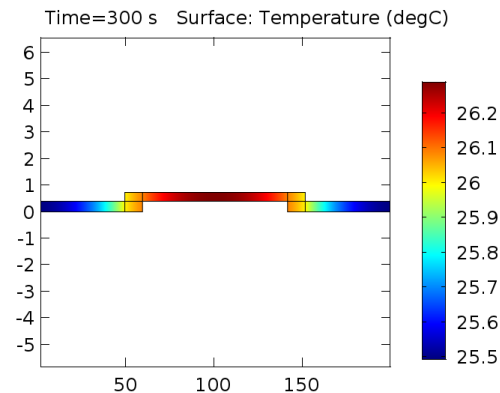
- Results show a good match. They also help in deciding the value of the convection coefficient of the system
- Temperature is higher at the welds than the centre of the foils

Predictions : Ni-Li system + thicker tabs

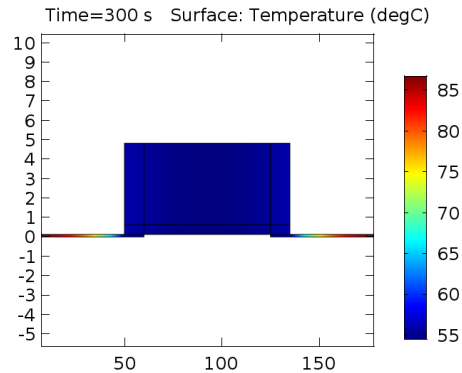
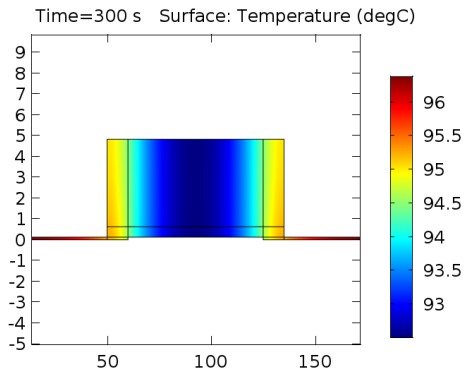
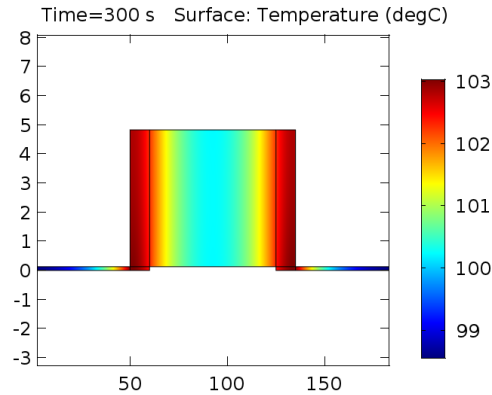
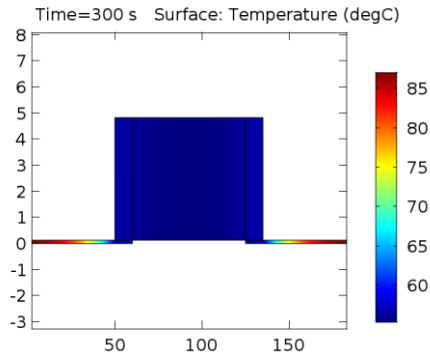


Temperature as a function of different currents across Ni-Li coupon system . Current is passed for 5 mins. Ni tabs are 0.1 mm and 0.4 mm thick.

- Nickel-Lithium systems shows a much higher temperature
- Thicker tabs leads to lower tab resistance and the maximum temperature shifts to the centre of the foils

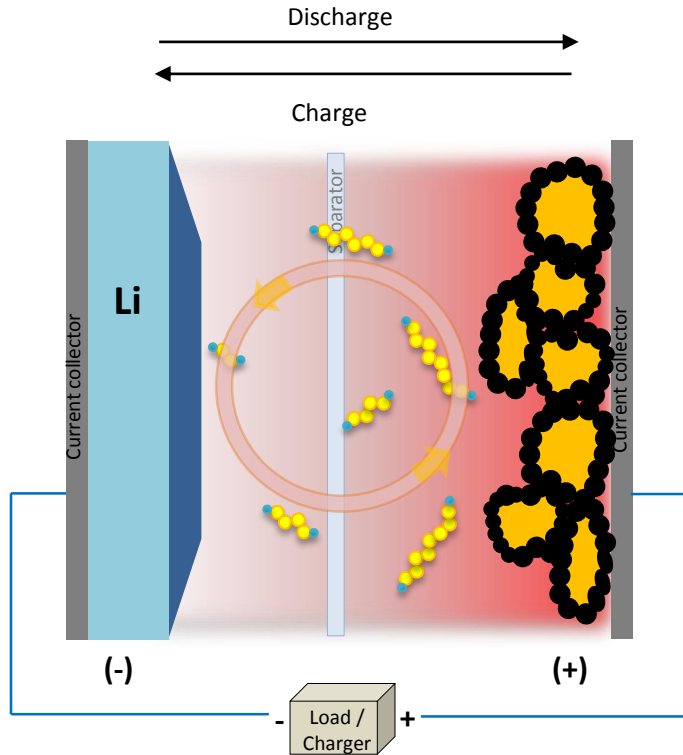


Temperature gradient across the Al system with Al tabs = 0.4 mm at 300 s when 40 A is passed through it. Figures are rescaled in the y direction

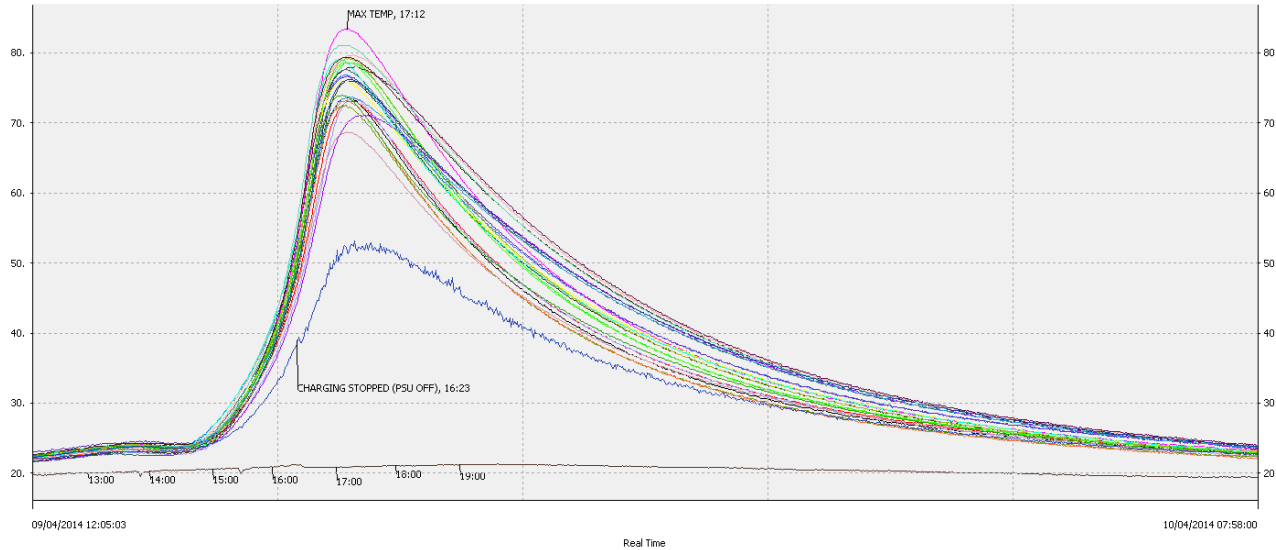
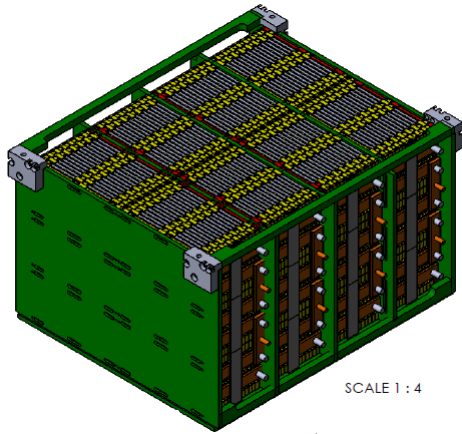


- Increasing the resistance by an order of magnitude leads to the maximum temperature shifts to the weld spot : In short the weld resistance as to be of the same order as the tab resistance to have a noticeable effect
- If the resistance is moved upwards, the current doesn't pass through it and therefore the temperature rise is not as great : issues with setup

- Cell Design : Weld resistance
- **Battery Pack : Polysulfide shuttle and thermal runaway**
- Pack Integration : Laminar Flow



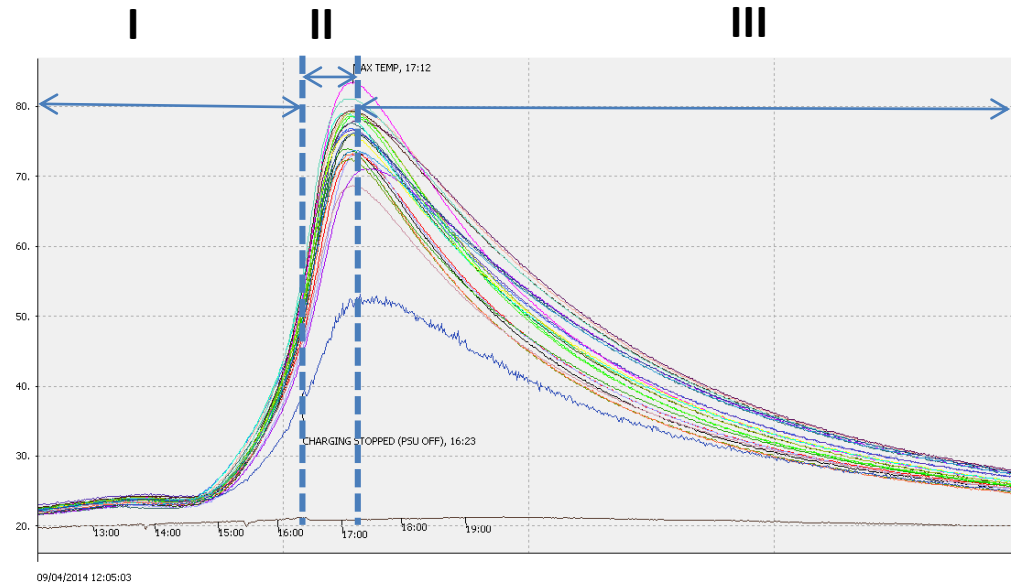
- During discharge sulfur reduces to lower order polysulfides, with the reverse for charging
- During charge these polysulfides move to the anode, where they get converted to the higher order polysulfides and migrate back to the cathode : parasitic current
- This phenomena leads to an increase in temperature : starts a vicious cycle of increasing the oxidation at the anode and making the parasitic current even larger
- Happens during charge at higher voltages



- As the battery pack was being charged, a sudden increase in temperature was noticed
- Charging was stopped, but the temperature continued to rise, reaching a peak of 80 °C
- After being left overnight, the battery cooled down to ambient temperature

Li-S Battery pack : Polysulfide Shuttle

- The curve can be broken into three parts : The first where charging occurs.
- The second where self discharge due to polysulfide shuttling occurs : and will continue to generate heat causing the temperature to rise
- The third is just air cooling
- This modelling was achieved with the Heat Transfer module coupled with Global ODE's and Events



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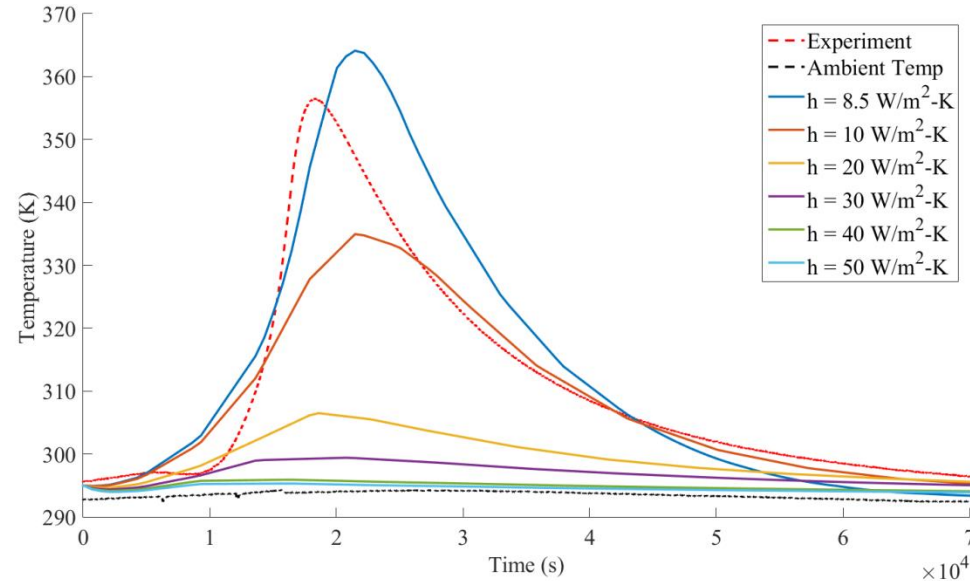
- The full form of the equation of formation of polysulfides can be expressed as (Mikhaylik and Akridge, 2004)

$$\frac{\partial [c_p]}{\partial t} = i_{charging} - k_s [c_p]$$

- The shuttle constant itself can be expressed as dependant on temperature
- During polysulfide shuttling, the heat generation term is directly proportional to the shuttle current ($V I_c$, where V would be the charging voltage, I_c the charging current)
- Hence the heat generation term is dependant on the shuttle constant as well as the polysulfide concentration : this is responsible for the bell shaped curve

$$\dot{q} = B k_s [c_p]$$

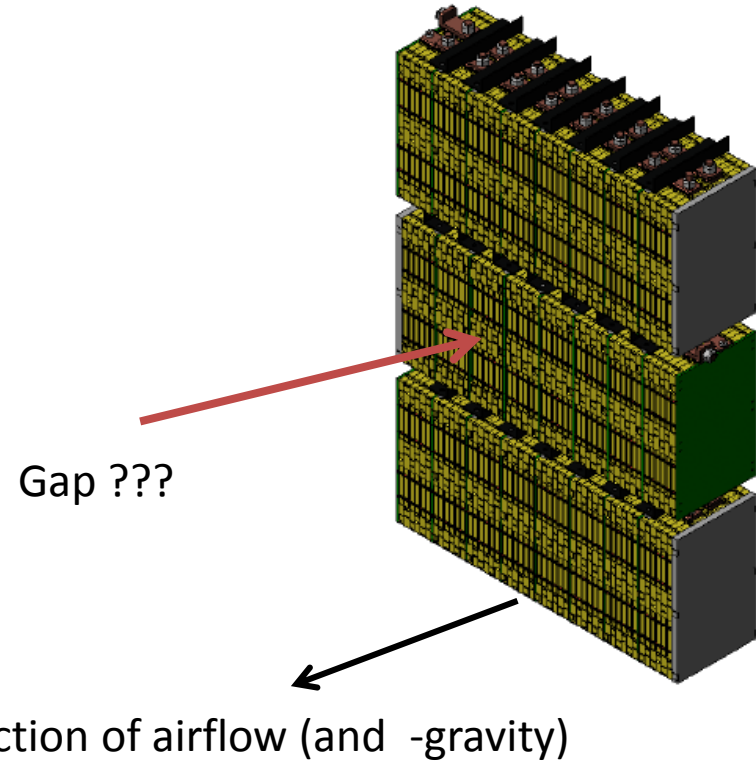
- Initial fit gets the shape approximately
- It is likely that the shuttle current during charging is not a constant, like has been used here, but changes with the change of concentration gradients in the cell.
- Cooling is required as a precaution for such an event : however might need a more robust system than forced convection



- Cell Design : Weld resistance
- Battery Pack : Polysulfide shuttle and thermal runaway
- **Pack Integration : Laminar Flow**

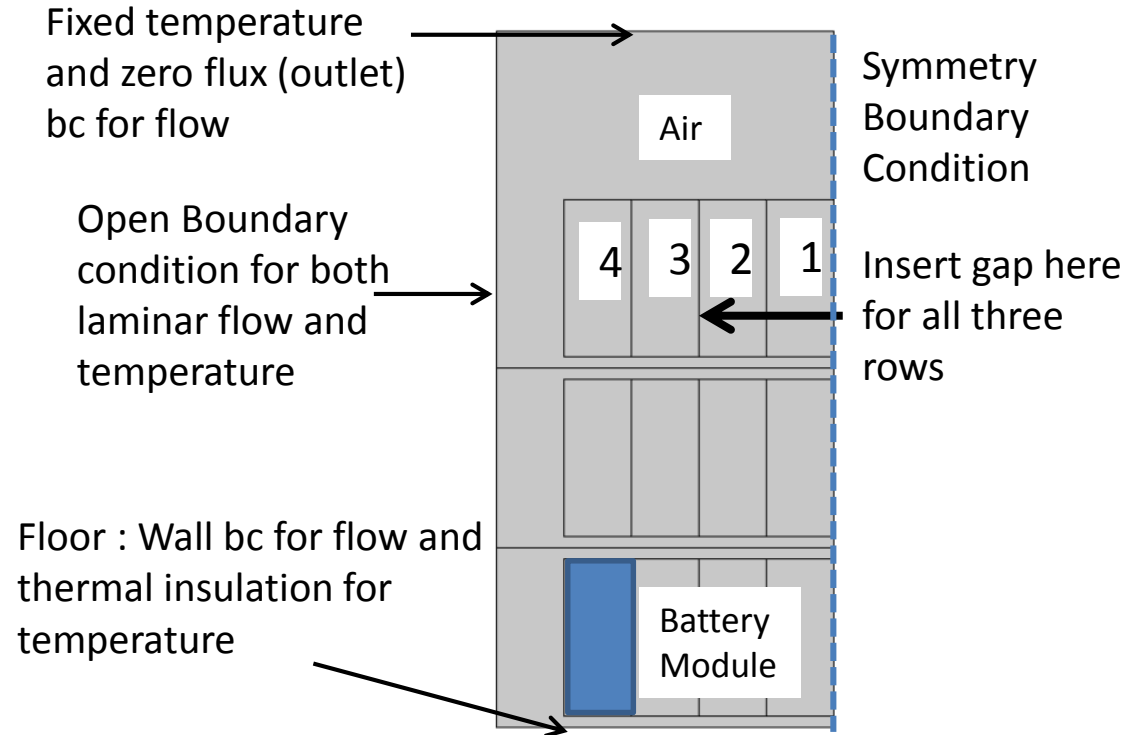
Rack Mounted Battery

- Series of Modules which can be put on a rack
- Question : Should there be a gap between individual modules to allow for better air flow, and therefore better temperature control
- For this model , laminar flow was used in conjunction with the Heat Transfer in Solid modules and global ODE's to solve the polysulfide equation
- The model developed for polysulfide shuttle earlier was used for this simulation

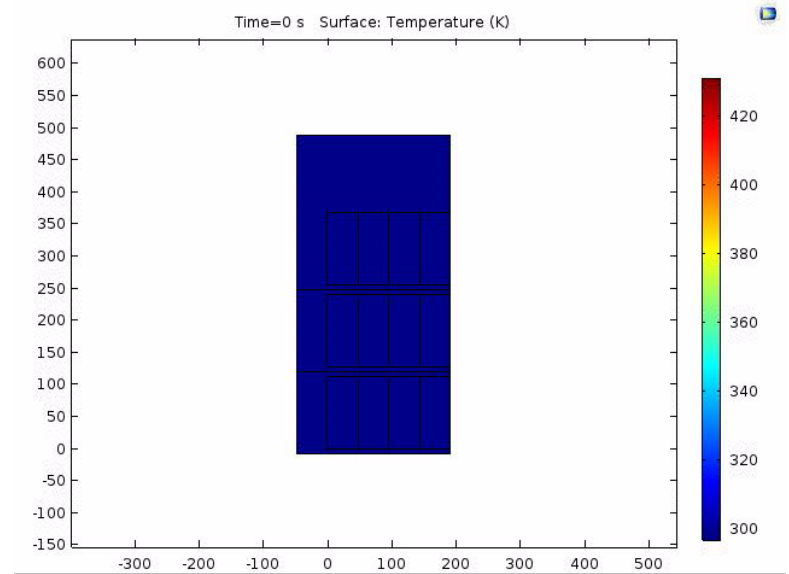
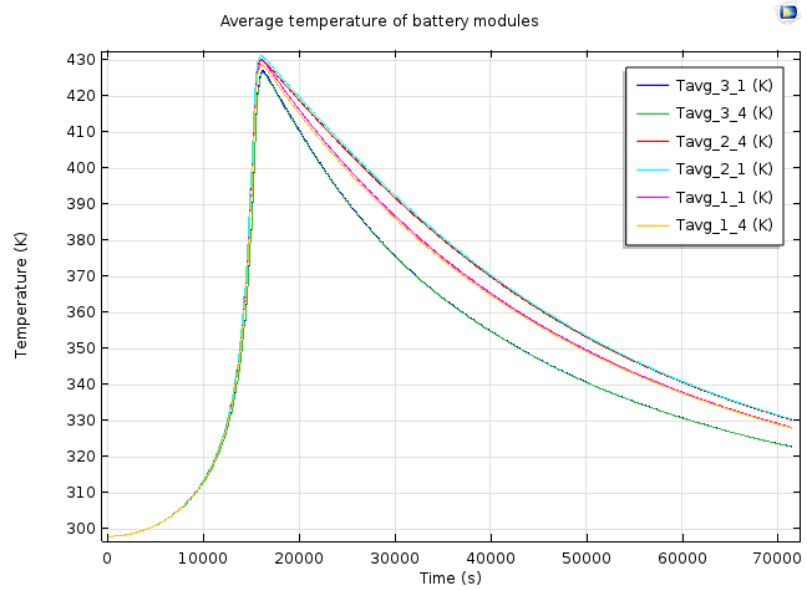


Layout of geometry

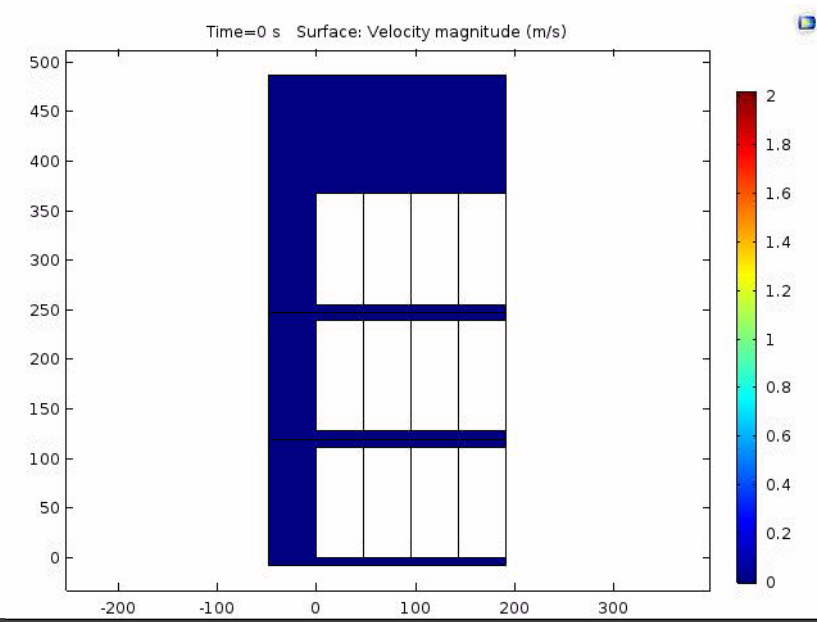
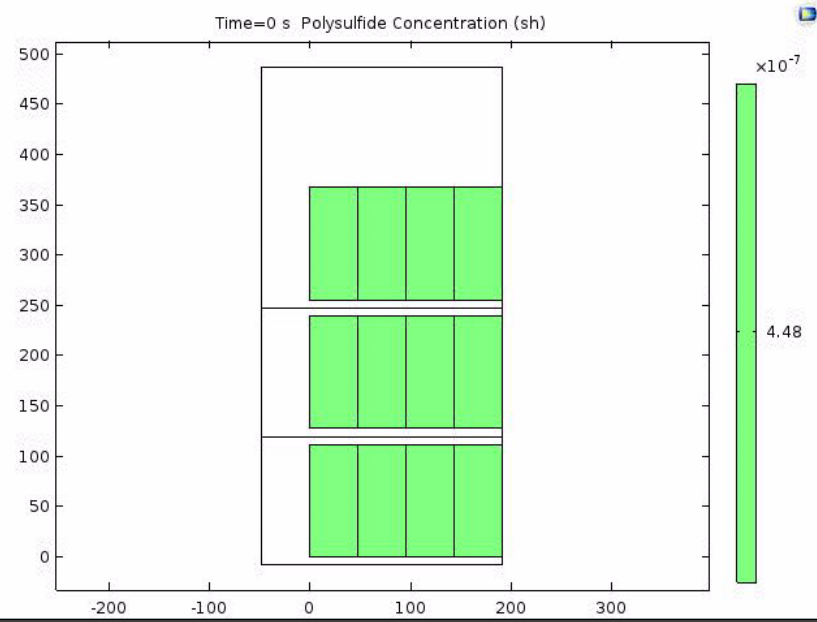
- We look at effect of **Free convection**, natural airflow where buoyancy forces due to gravity cause mixing of air
- 3D simulations have difficulty converging, therefore we revert to a 2-D configuration
- For this simulation we assume a continuous battery box in the through thickness direction



- The shuttle heat source is not constant, we use the same parameters as for the solar cell battery
- The temperature rise is similar, the fall is different due to geometry

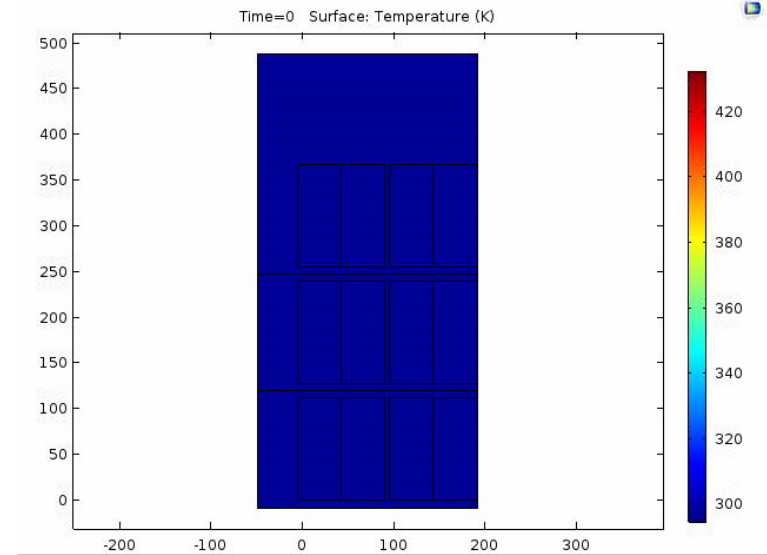
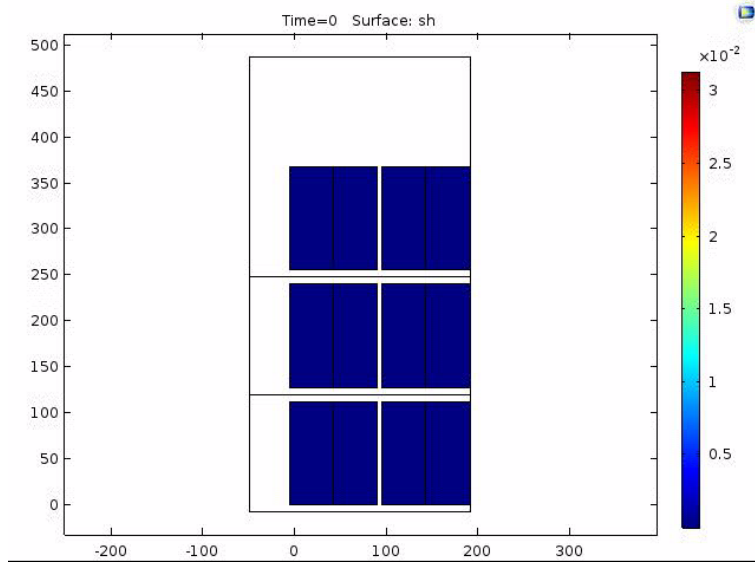


- Polysulfide concentration depends on charging current and temperature.
- The concentrations are similar during heating , but vary as the rate of cooling changes in the different battery packs : Implications for SOC



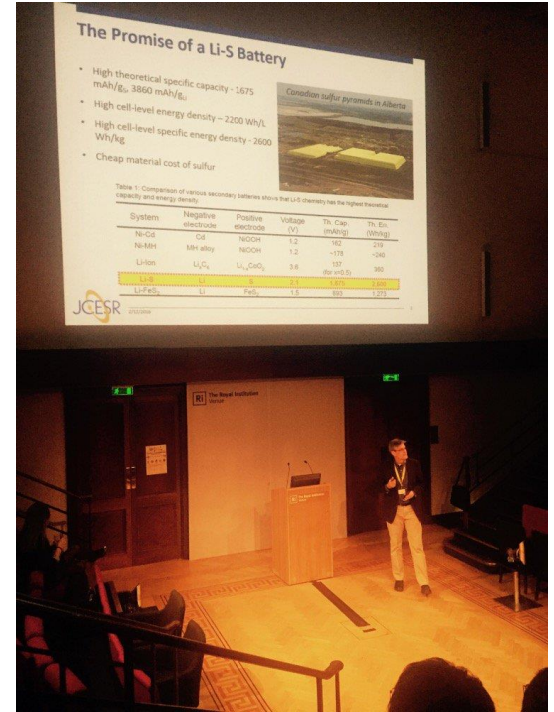
Shuttle Heat Source : Gap

- The temperature of the inner modules are almost identical to the situation with no gap present. However the outer modules do show lower temperatures, this is also reflected in the polysulfide concentration

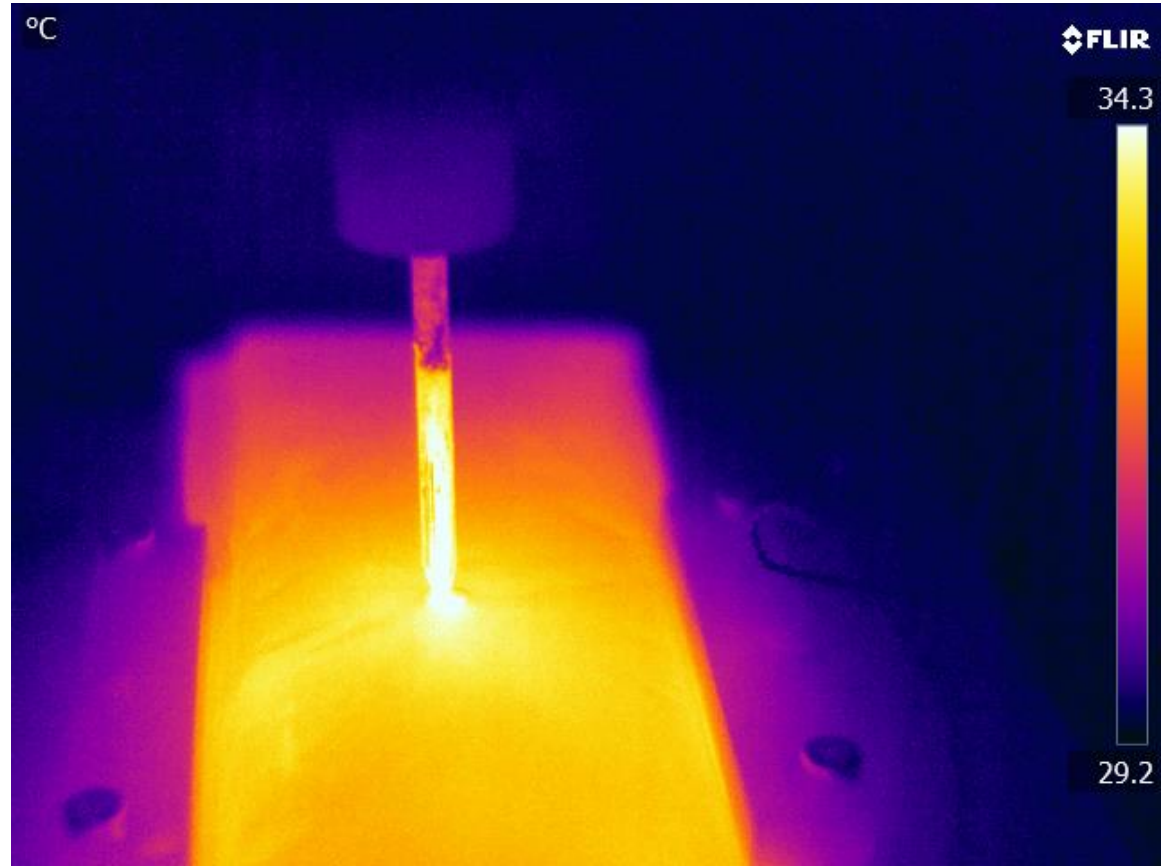


- Lithium sulfur is a new and exciting system for energy storage
- Along with modelling the electro-chemistry, issues related to scaling up and commercialising this technology need to be addressed e.g. Thermal issues
- Modelling is a good way to expedite this process and catch up to where lithium ion is relatively rapidly
- COMSOL is well suited for this as the multiphysics nature of the package allows for coupling several different phenomena simultaneously
- Weld resistance as of now is not an issue with OXIS cells
- Polysulfide shuttle is a serious issue and a combined approach of better design and cooling is required in order to mitigate its effects

- Li-SM3 Conference on 26th – 27th April 2017, IET Savoy London. For details please check out www.lism3.org
- M-M-M : Materials , Mechanisms and Modelling
- Special emphasis on use of modelling to solve issues
- All three joined together with industry to discuss Applications



- The REVB Team
 - Dr Geraint Minton
 - Dr Sylwia Walus
 - Dr Mark Wild
 - Tom Cleaver
 - Dr Peter Kovacic
- R&D, OXIS
 - Dr Laura O'Neill
 - Dr David Ainsworth
- Imperial College
 - Dr Greg Offer
- Cranfield University
 - Dr Daniel Auger
- Ricardo



- Following Mikhaylik and Akridge, 2004, one can plot the change in concentration of the polysulfides as a function of time during self discharge following the expression

$$\frac{\partial [c_p]}{\partial t} = -k_s [c_p] \quad [c_p] = [c_p^0] e^{-k_s t}$$

- Where k_s is the shuttle constant
- Hence, if we state that the heat generation term is proportional to the concentration of polysulfides it is possible to write it as

$$\dot{q} = A e^{-k_s t}$$

- Where A and k_s can be fitted
- Polysulfide concentration was calculated as a global ODE with a fit for the shuttle constant k_s

- If there was forced air cooling, e.g. a fan, the convective coefficient increases by an order of magnitude at least.
- Simple simulations show that the cooling period is reduced for 14 hours to approximately 3 hours
- There is also a reduction of the peak temperature reached.
- For an exothermic event though, even more aggressive cooling might be required

