

# Simulation of Mass Transfer in a Microfluidic Experiment Using the Moving Mesh Method

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# Modeling of Microreactors

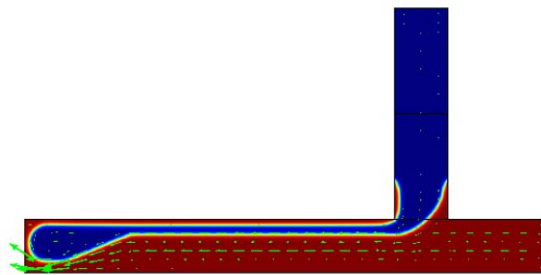
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- Two phase liquid-liquid systems are used extensively in chemical processes
- Microfluidics promises high mass transfer rates and compactness
- Optimization of a microreactor system must address numerous configuration options and operating parameters
- Progress has been made toward characterization of two-phase flow
- Need a definitive set of experiments to validate microfluidic mass transfer model
- Modeled Burns – Ramshaw experiments

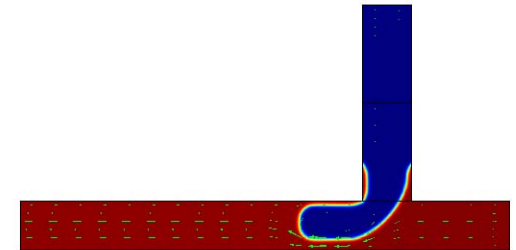
# Initial Attempts to Model Experiments With COMSOL

Provides solutions that describe the interaction between multiple physical systems

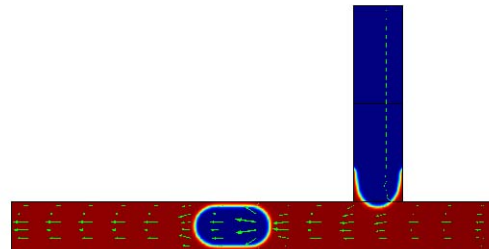
- Phase Field method
  - Provides improved phase conservation compared to Level Set
  - Mobility parameter allows matching of L/D of slugs



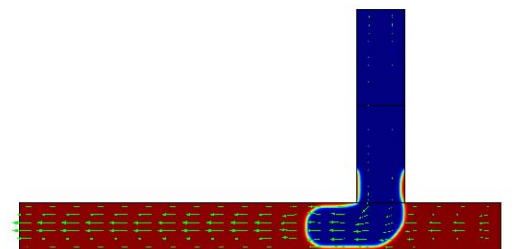
(a) Mobility Parameter = 10



(c) Mobility Parameter = 1000



(b) Mobility Parameter = 100



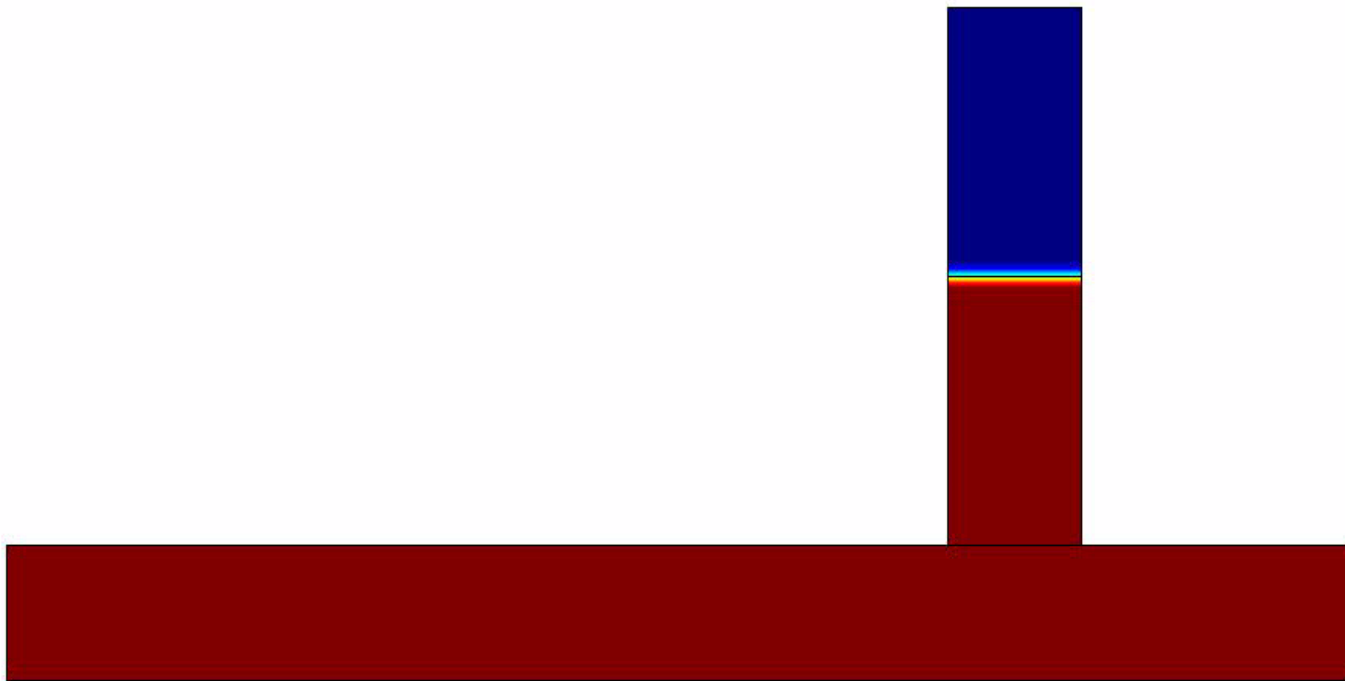
(d) Mobility Parameter = 10,000

# Initial Attempts to Model Experiments (Continued)

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The dispersed phase can undergo spontaneous shrinkage with Cahn-Hilliard formulation in the Phase Field method

Time=0 Surface: Volume fraction of fluid 1 (1)



# Initial Attempts to Model Experiments (Continued)

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Spontaneous phase generation can also occur

Time=0 Surface: Volume fraction of fluid 1 (1)



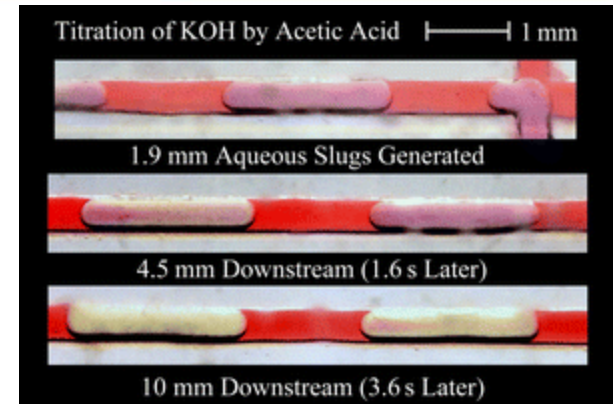
# COMSOL – Moving Mesh Method

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- Uses an Arbitrary Lagrangian-Eulerian Formulation (ALE)
- Advantages
  - Phases are conserved
  - A discrete phase boundary allows specification of species locations and partition coefficient
  - Slug deformation based upon physical forces
- Disadvantage
  - Will not model formation of fluid slugs

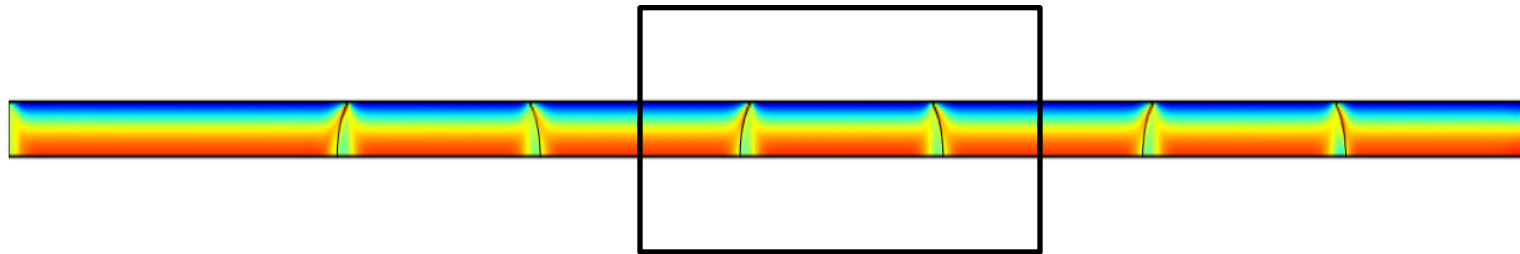
# Case Study – Burns - Ramshaw Experiments

- Experimental conditions:
  - 0.38 mm square channel
  - Kerosene contains 0.5 M acetic acid
  - Water contains 0.25 M KOH
  - Flow velocity = 2.8 mm/sec
  - Acetic acid prefers aqueous phase  
( $P = C_o/C_w = 0.036$ )
- Modeled with moving mesh method
  - Contact angles modeled with Navier slip boundary condition
  - Distribution coefficient implemented with stiff spring method
  - Reaction between KOH and acetic acid modeled

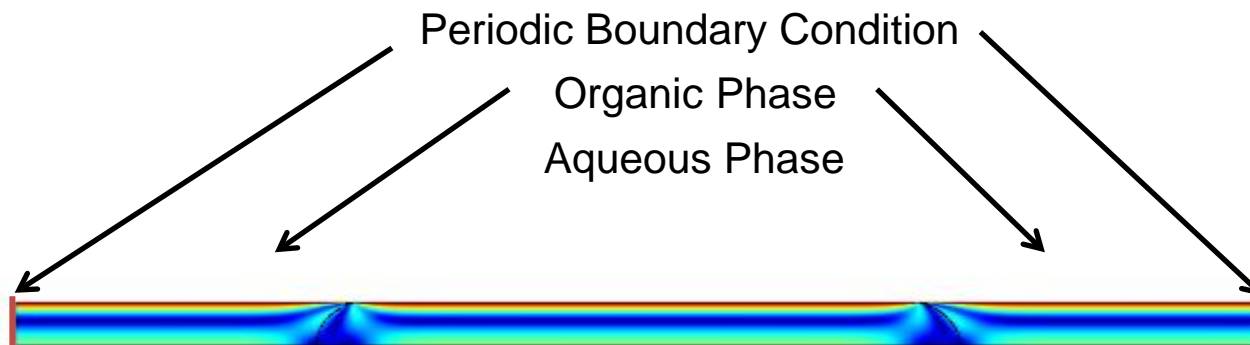


# Moving Mesh – Two step method

- Fluid dynamics is solved first



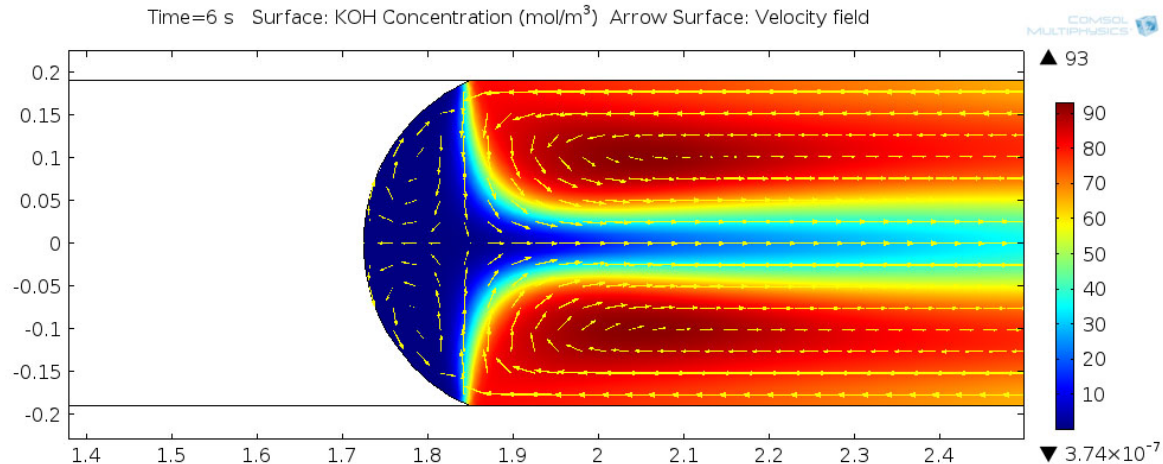
- Mass transfer solved under steady-state flow



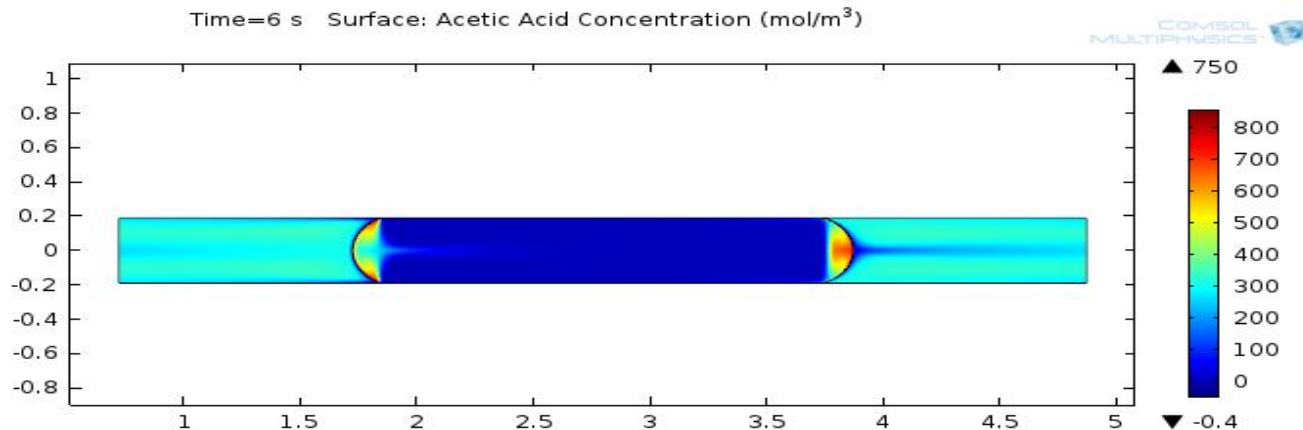


# Characteristics of Flow at Interface

- Development of secondary flow pattern

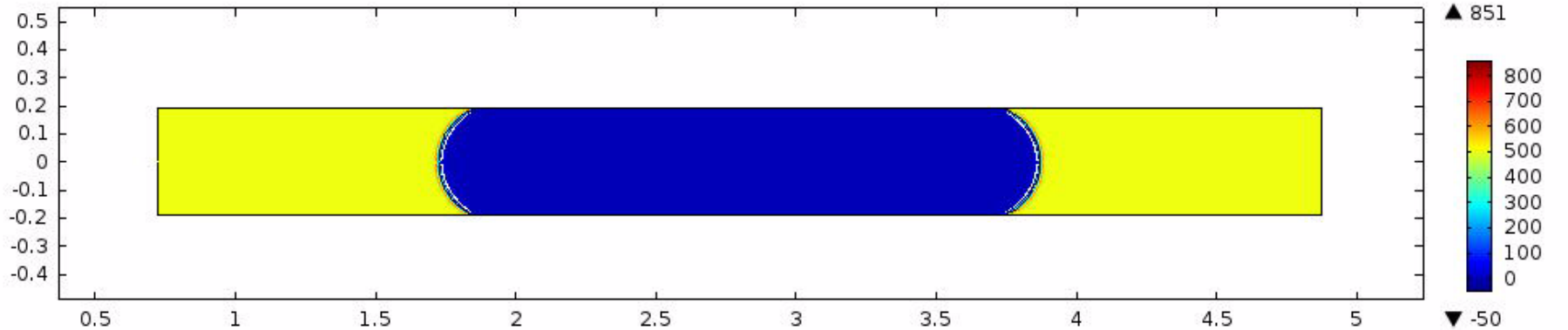


- Partition coefficient and inhibited mass transfer

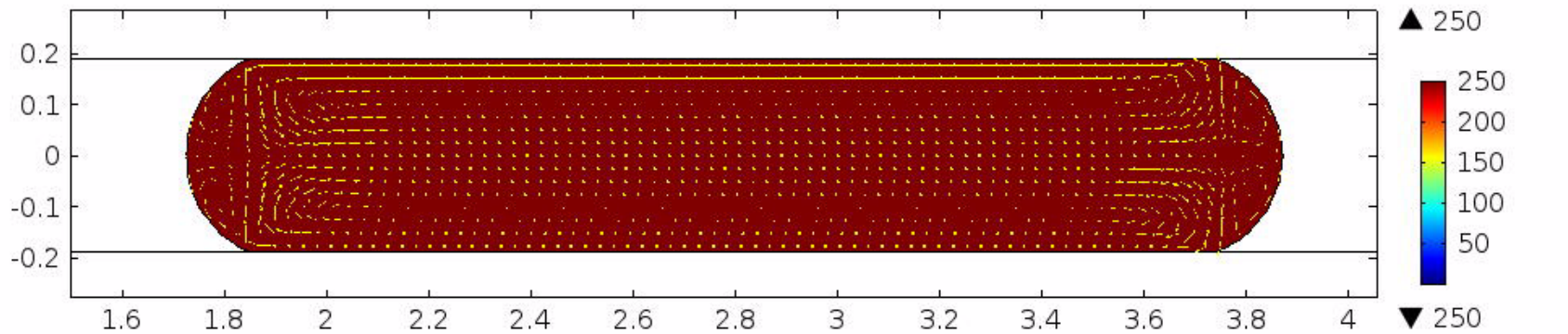


# 2D - Simulations

Time=0 s Surface: Acetic Acid Concentration (mol/m<sup>3</sup>)



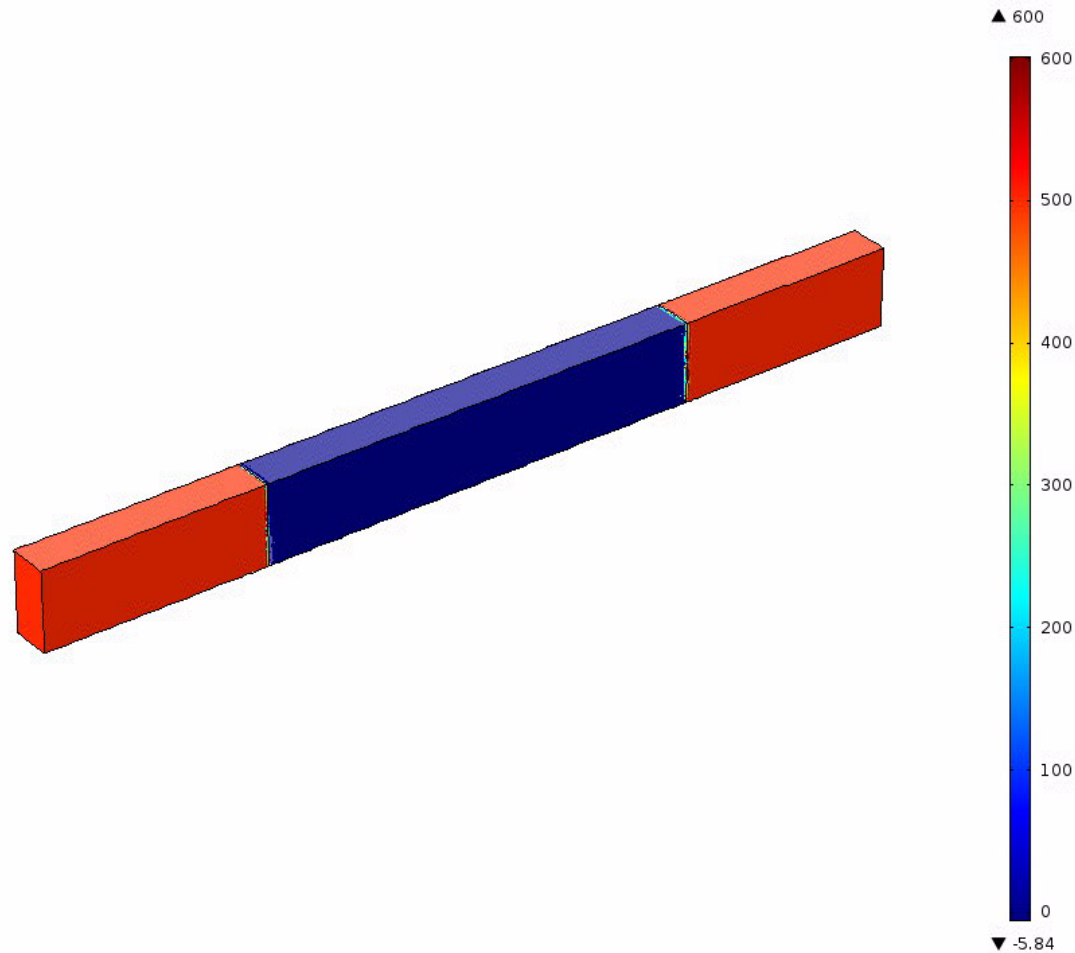
Time=0 s Surface: KOH Concentration (mol/m<sup>3</sup>) Arrow Surface: Velocity field



# 3D Simulation for Acetic Acid Concentration

Time=0 s Surface: Acetic Acid Concentration (mol/m<sup>3</sup>) (mol/m<sup>3</sup>)

COMSOL  
MULTIPHYSICS

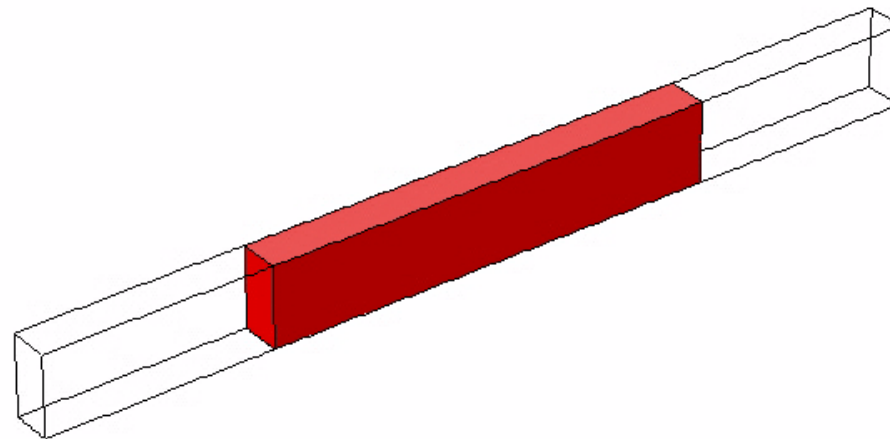


# 3D Simulation for Potassium Hydroxide Concentration

Time=0 s Surface: KOH Concentration (mol/m<sup>3</sup>)

COMSOL  
MULTIPHYSICS

▲ 250



250

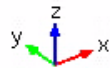
200

150

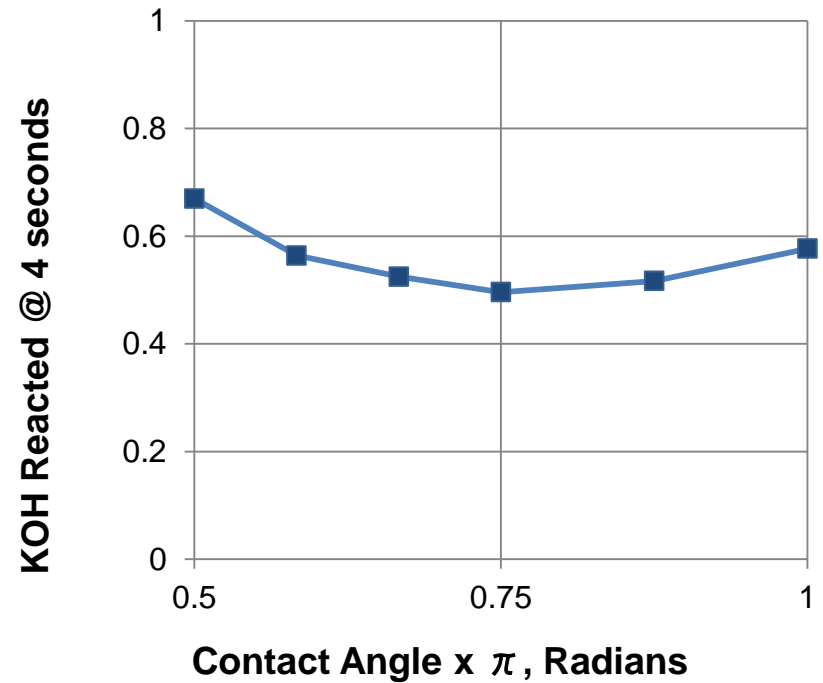
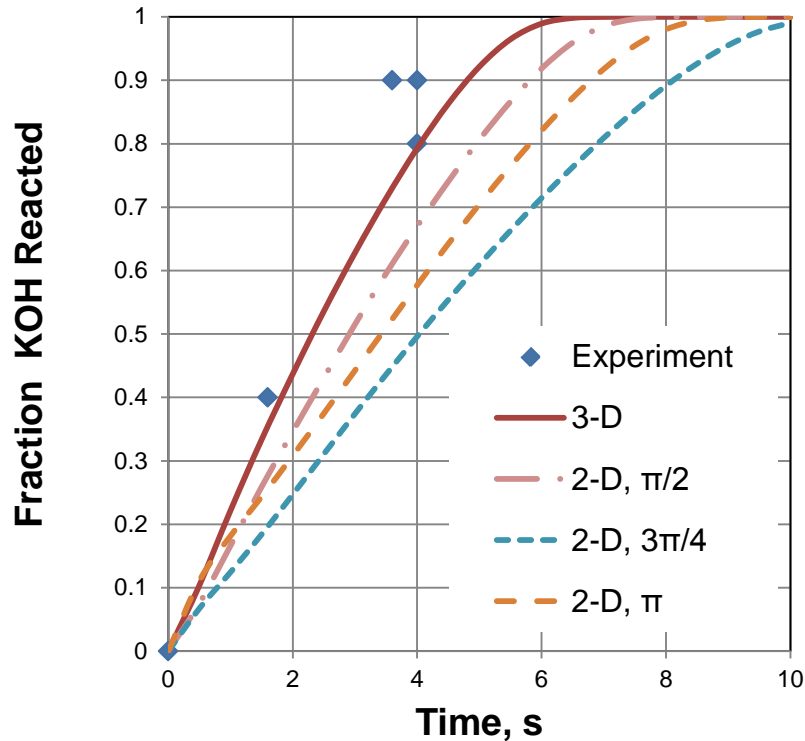
100

50

▼ 249



# 2D Contact Angle & 3D Model



# Summary and Future Work

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- Level set and Phase Field method model slug formation
  - Lack of discrete boundary creates challenge for mass transfer
- Moving mesh method
  - Does not model slug formation
  - Effectively models mass transfer
- Validated predictions provide basis for simulating experiments
- Improvement in 3-D re-meshing is needed to maintain element quality at contact angle  $\neq \pi / 2$