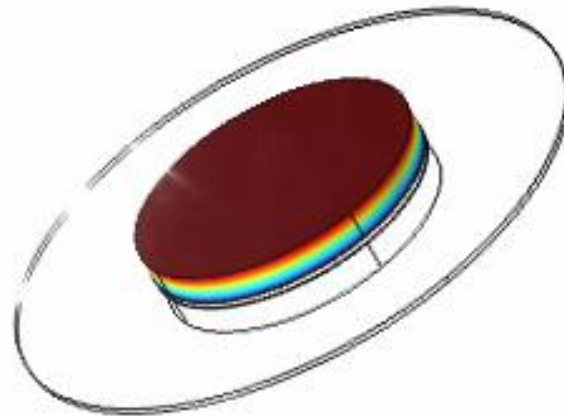


Parametric Study of Electrolyte-Supported Planar Button Solid Oxide Fuel Cell

R. Gentile, A. Aman, Y. Xu, N. Orlovskaya



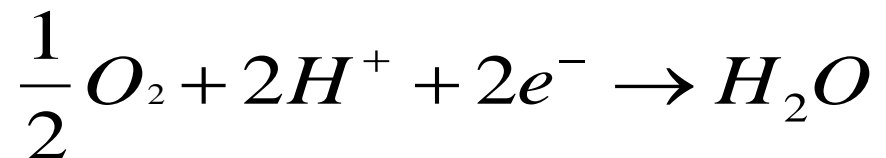
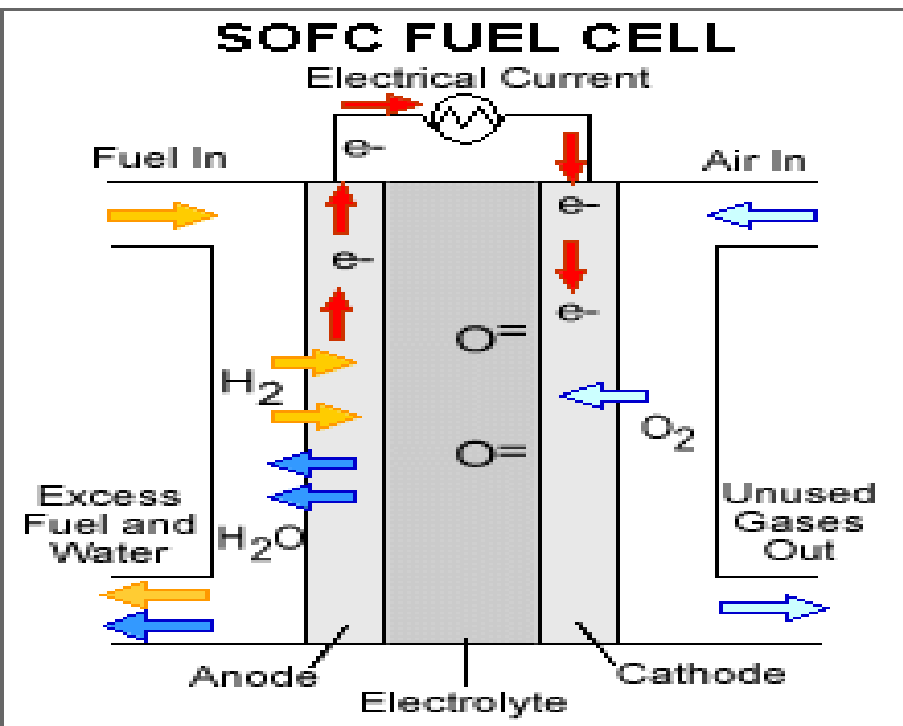
Solid Oxide Fuel Cell (SOFC)

SOFC


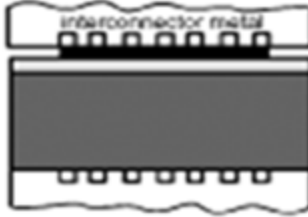

- ✓ Solid electrolyte - Ceramics
- ✓ Operating temperatures (400°C – 1000°C)

Advantages of SOFC

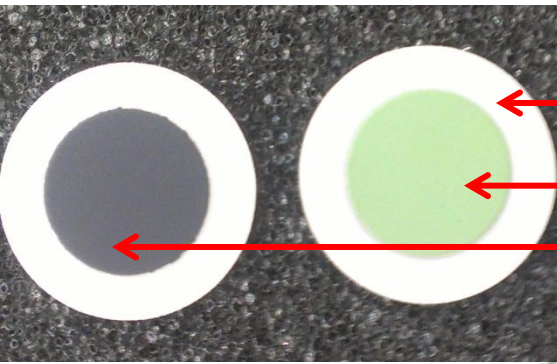
- ✓ High efficiency (>50%, >80% CHP)*
- ✓ Fuel flexibility (H₂, natural gas, biogases, etc.)
- ✓ Combined Heat & Power generation
- ✓ Compatible with gas & steam turbines
- ✓ Power output (W to MW)
- ✓ Relatively higher power density
- ✓ No water flooding issues, unlike PEMFC



Types of Planar SOFC

<i>Cathode-supported</i>	<i>Anode-supported</i>	<i>Electrolyte-supported</i>
<p>700-800°C</p> 	<p>700-800°C</p> 	<p>1000°C</p> 
Cathode: 300 - 1000 μm	Cathode: 50 μm	Cathode: 50 μm
Electrolyte: < 20 μm	Electrolyte: < 20 μm	Electrolyte: > 100 μm
Anode: 300 – 1000 μm	Anode: 500 - 1500 μm	Anode: 50 μm
<p>Activation losses higher than Anode-supported</p>	<p>Higher Activation losses</p>	<p>Higher Ohmic losses</p>

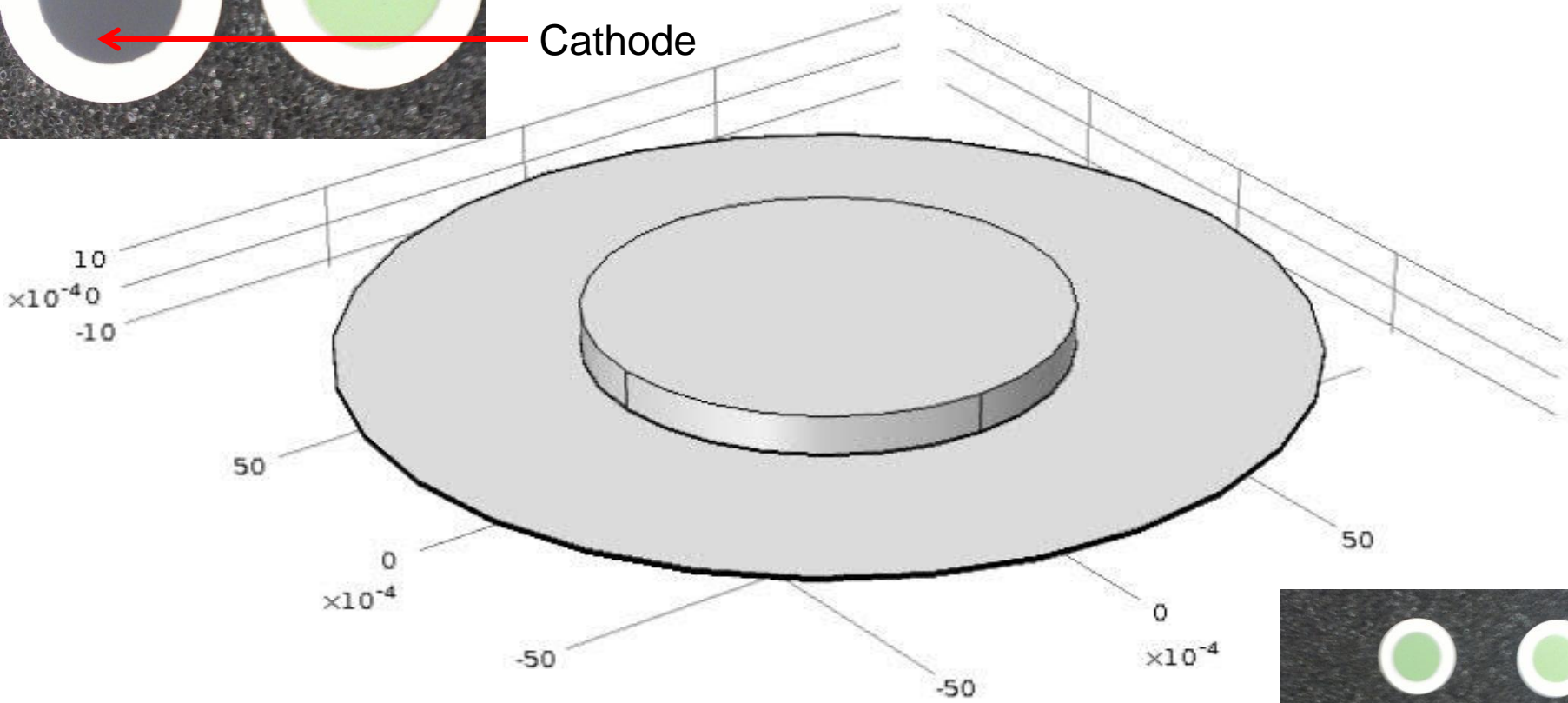
SOFC Geometry: Top View



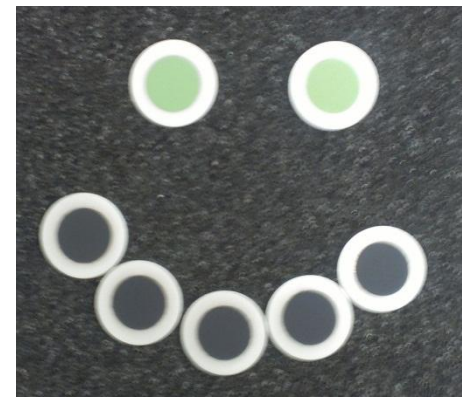
Electrolyte

Anode

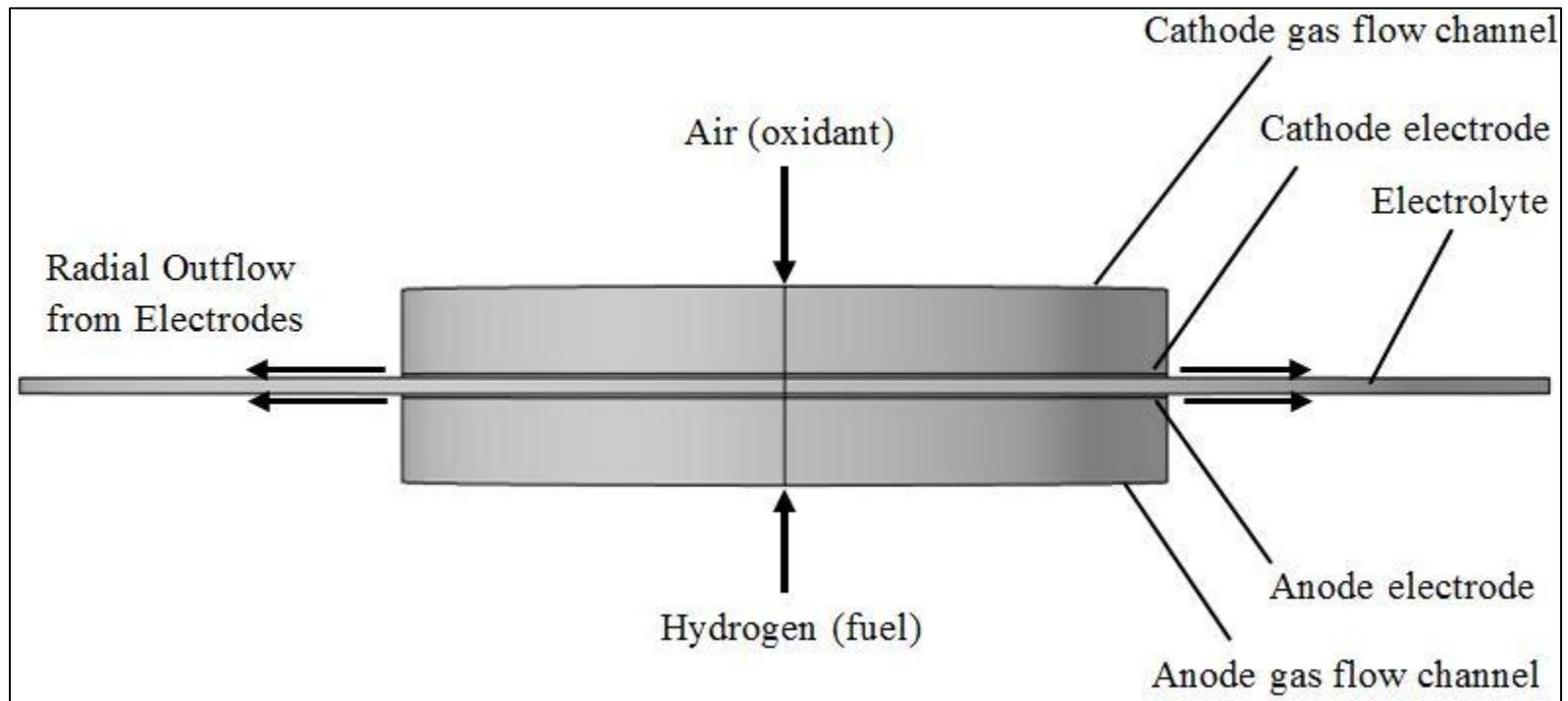
Cathode



all units in m



SOFC Geometry



Anode & Cathode thickness	50 μm
Electrolyte layer thickness	30 μm
Anode & Cathode diameter	10 mm
Electrolyte diameter	20 mm
Gas flow channel height (Anode & Cathode)	1 mm
Gas flow channel diameter (Anode & Cathode)	10 mm

Parametric Study

- SOFC modeling involves a large number of parameters that affect the cell performance.
- These parameters affect different aspects of the cell's performance and hence it is important to study them individually.
- By this process, the parameters can be narrowed down to a few that have a significant impact and influence on the cell's behavior.

j_0 (A/m²), exchange current density

SSA (m²/m³), specific surface area

σ (S/m), electrolyte conductivity

ε , electrode porosity

k , electrode permeability

t (μ m), electrode thickness

Exchange Current Density (ECD) and Specific Surface Area

Butler-Volmer equation:

$$j = j_0 \left[\left(\frac{c}{c_0} \right)_R \exp \left\{ \frac{n\alpha F}{RT} \eta \right\} - \left(\frac{c}{c_0} \right)_P \exp \left\{ \frac{-n(1-\alpha)F}{RT} \eta \right\} \right] \quad \begin{array}{l} n = 2, \text{ anode} \\ n = 4, \\ \text{cathode} \end{array}$$

$$j_0 = A_v \cdot j_{local}$$

j = current/area [A/m^2], current density vector

j_0 – exchange current density

A_v – specific Surface Area [m^2/m^3]

η – activation overpotential [V]

c_R, c_P – concentration of reactants & products respectively

n : number of charges transferred

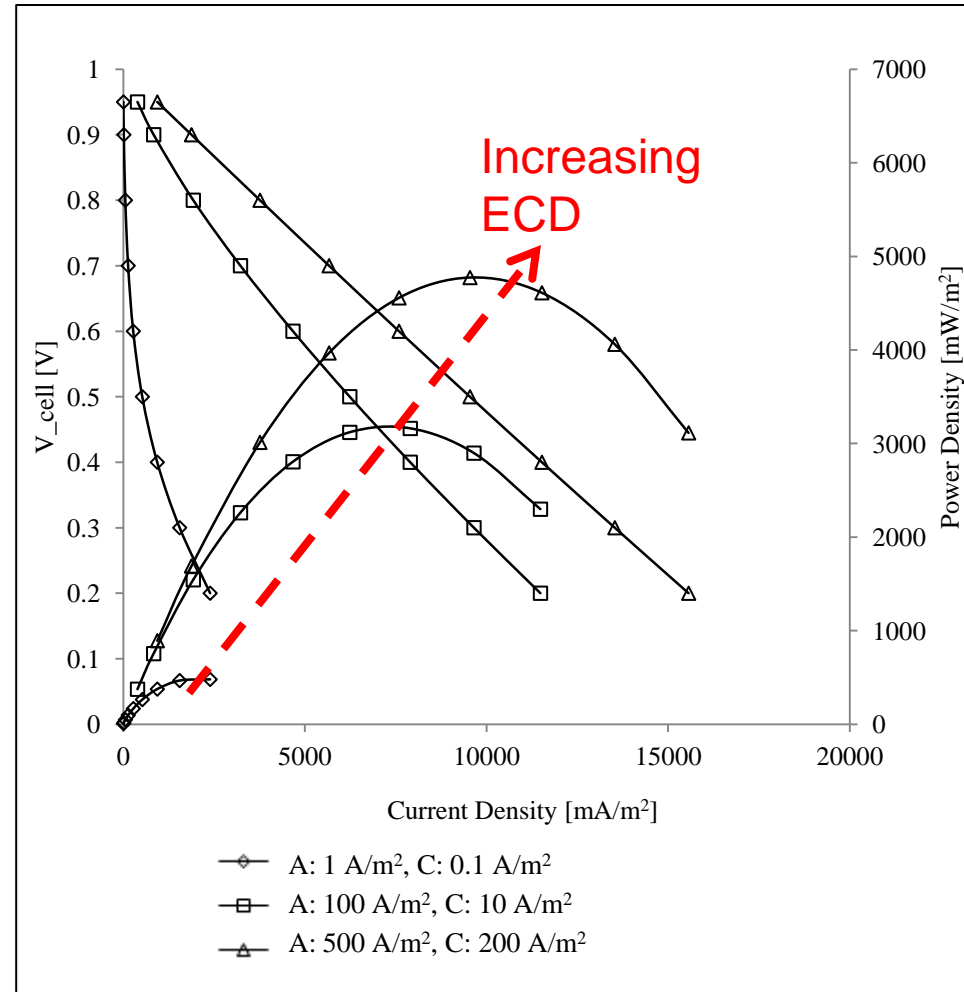
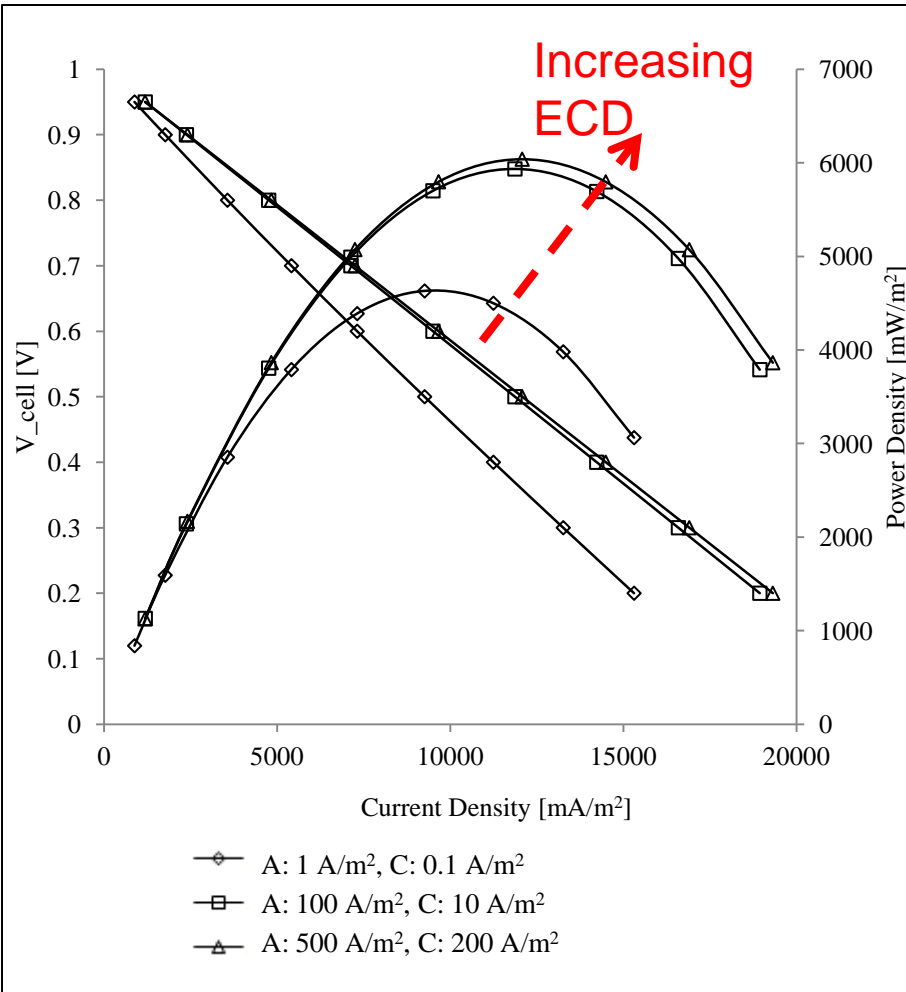
α : transfer coefficient

T : temperature (K)

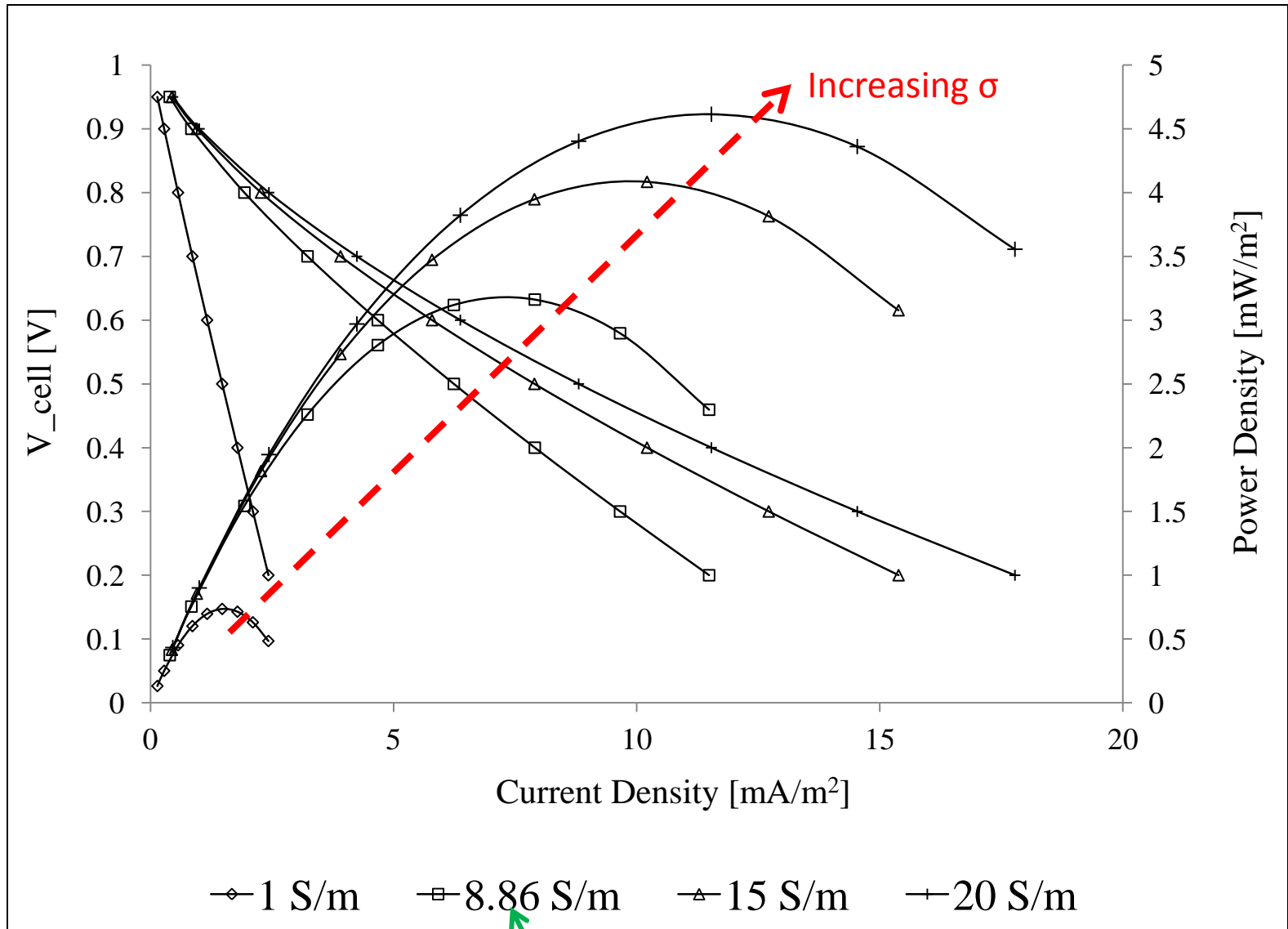
Exchange Current Density

SSA: 1×10^9 [m²/m³]

SSA: 1×10^6 [m²/m³]

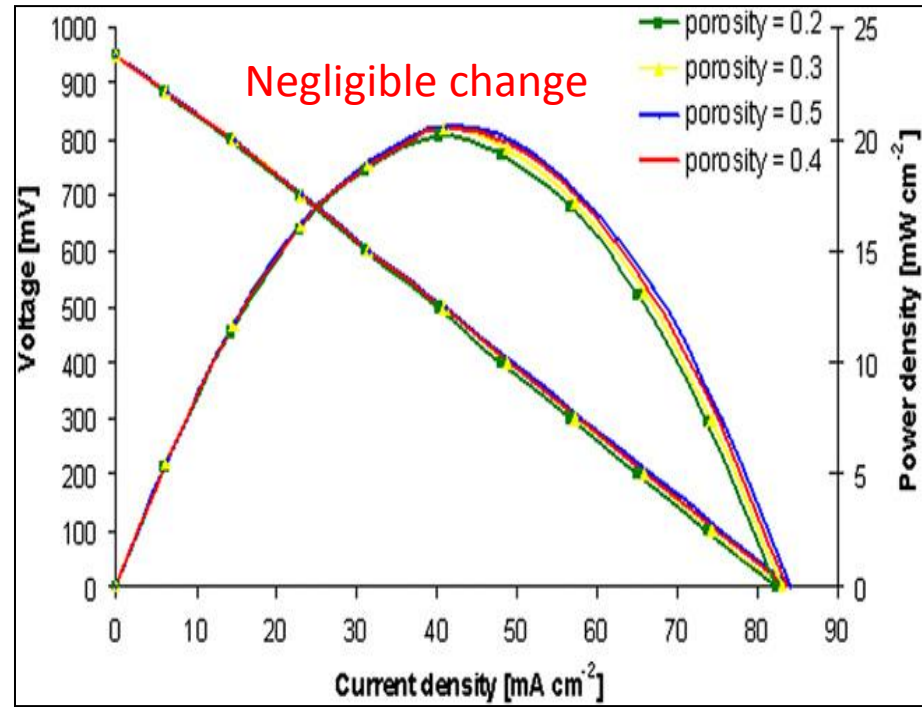
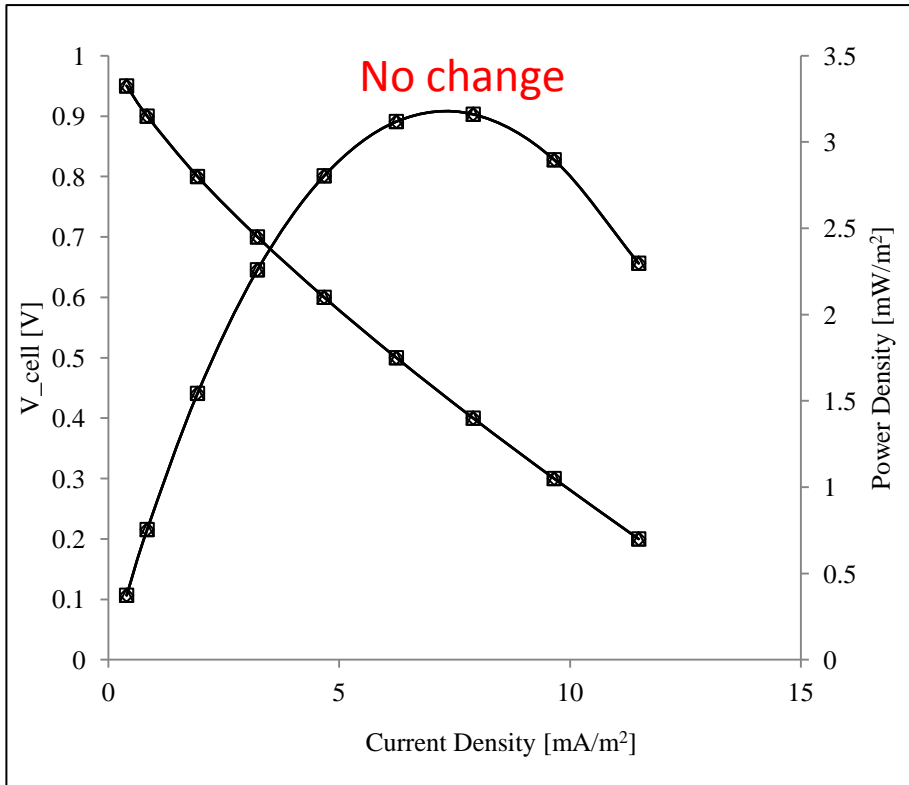


Electrolyte Conductivity



Conductivity of electrolyte produced at our lab

Electrode Porosity – Comparison with Published Results

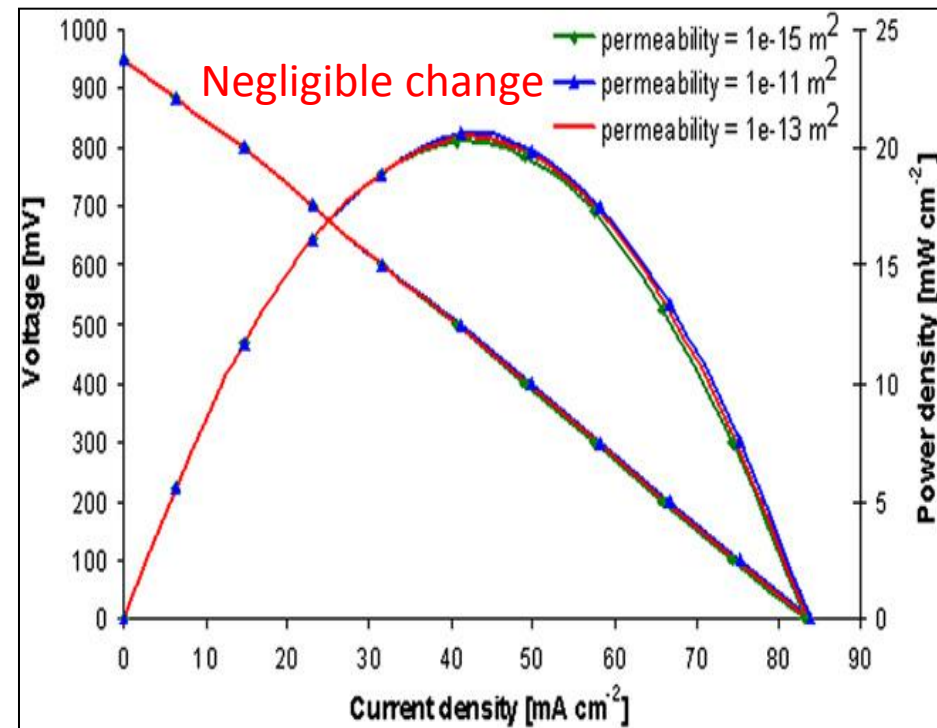
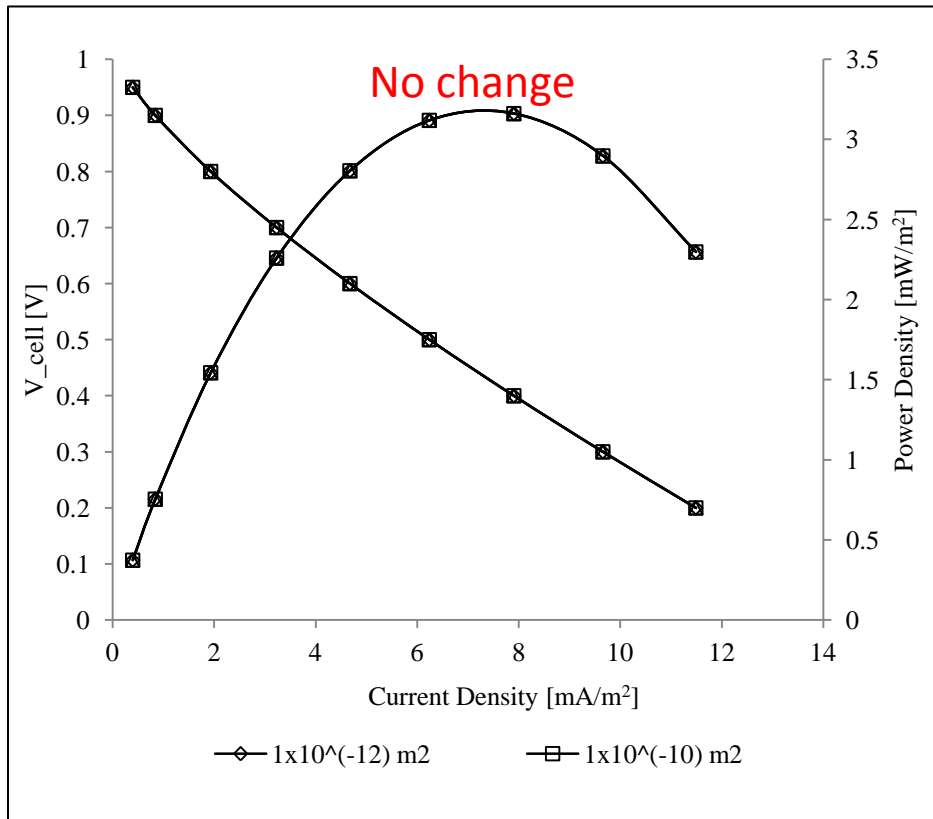


Akhtar et al., *International Journal of Hydrogen Energy*, 2011

$$\frac{\rho}{\varepsilon_p} \left(\frac{\partial u}{\partial t} + (u \cdot \nabla) \frac{u}{\varepsilon_p} \right) = -\nabla p + \nabla \cdot \left[\frac{1}{\varepsilon_p} \left\{ \mu(\nabla u + (\nabla u)^T) - \frac{2}{3} \mu(\nabla \cdot u)I \right\} \right] - \left(\frac{\mu}{k} + Q_{br} \right) u + F$$

ε_p : porosity

Permeability – Comparison with Published Results

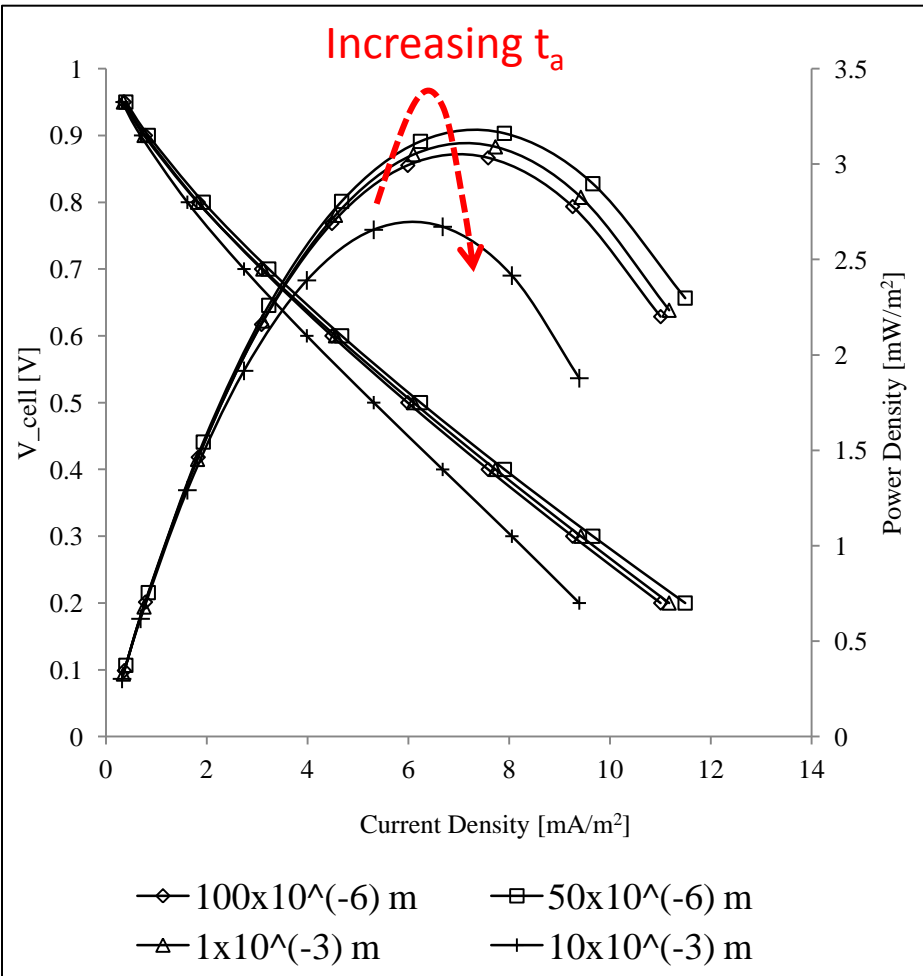


Akhtar et al., *International Journal of Hydrogen Energy*, 2011

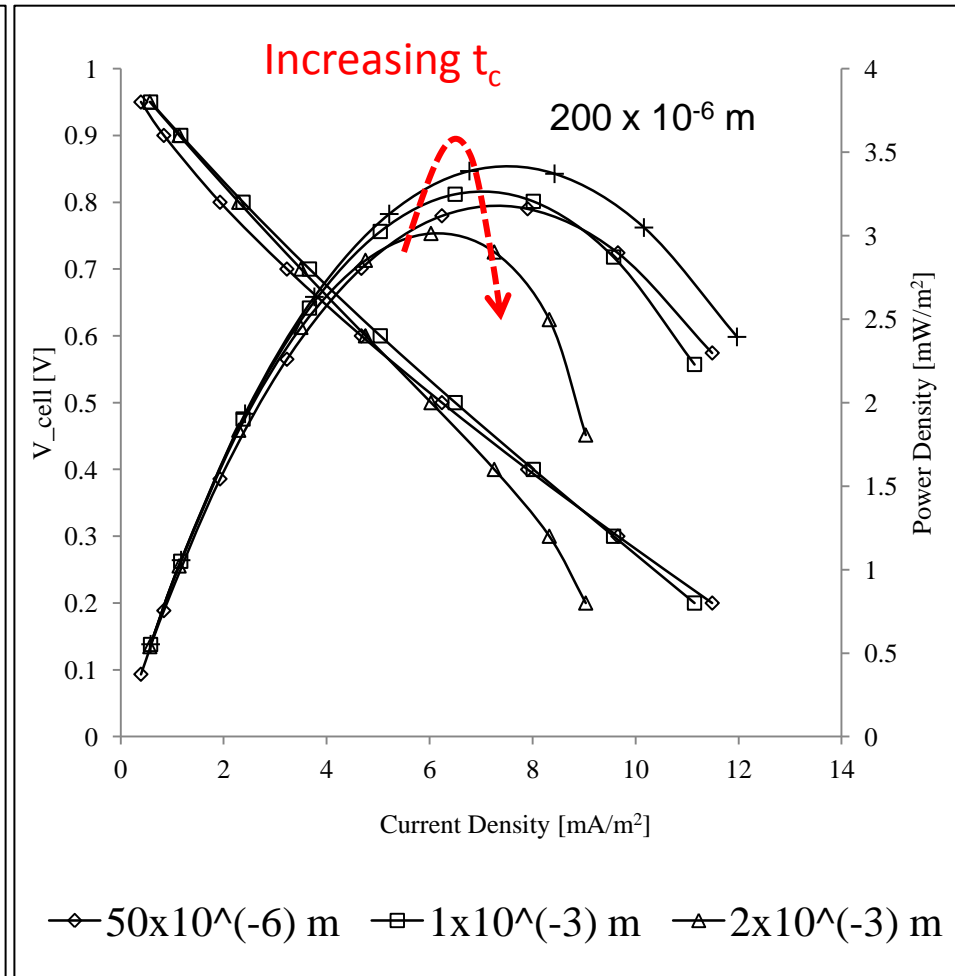
$$\frac{\rho}{\varepsilon_p} \left(\frac{\partial u}{\partial t} + (u \cdot \nabla) \frac{u}{\varepsilon_p} \right) = -\nabla p + \nabla \cdot \left[\frac{1}{\varepsilon_p} \left\{ \mu (\nabla u + (\nabla u)^T) - \frac{2}{3} \mu (\nabla \cdot u) I \right\} \right] - \left(\frac{\mu}{k} + Q_{br} \right) u + F$$

k : permeability of porous medium (m²)

Anode & Cathode Thickness



Anode thickness



Cathode thickness

Summary

#	Parameter	Range	Max % variation in Current or Power density
1	Viscosity - Anode	$1 \times 10^{-6} - 1 \text{ Pa} \cdot \text{s}$	< 1%
2	Viscosity - Cathode	$3 \times 10^{-7} - 10 \text{ Pa} \cdot \text{s}$	4.83%
3	Exchange current - Anode	0.01 - 100 A/m ²	42.80%
4	Exchange current - Cathode	0.001 - 0.1 A/m ²	253.60%
5	Specific Surface Area - Anode	$1 \times 10^6 - 1 \times 10^{12} \text{ m}^{-1}$	98.90%
6	Specific Surface Area - Cathode	$1 \times 10^6 - 1 \times 10^{12} \text{ m}^{-1}$	327.22%
7	Permeability - Anode	$1 \times 10^{-13} - 1 \text{ m}^2$	0
8	Permeability - Cathode	$1 \times 10^{-13} - 1 \text{ m}^2$	0
9	Electrolyte Conductivity	1 - 15 S/m	63.35%

Conclusion & Future Work

- **A parametric study was conducted to identify key parameters that affect cell performance**
- **Exchange current density, specific surface area and electrolyte conductivity affect the performance significantly**
- **The affect of electrode thickness is not fully understood**
- **It is not clearly understood why performance is not affected by porosity and permeability of electrodes**
- **Future work will include incorporating emperical data or theoretical relationships**

Questions?
Thank you!